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L86 ANSWER 1 OF 21 HCAPLUS COPYRIGHT 2003 ACS
 AN 2000:529221 HCAPLUS
 DN 133:149135
 TI Sequential separation of whey protein
 IN Mozaffar, Zahid; Ahmed, Salah H.; Saxena, Vinit; Miranda, Quirinus Ronnie
 PA Sepragen Corporation, USA
 SO U.S., 47 pp., Cont.-in-part of U.S. 5,756,680.
 CODEN: USXXAM
 DT Patent
 LA English
 IC ICM C07K016-04
 ICS C07K014-47; A23C009-12
 NCL 530366000
 CC 15-3 (Immunochemistry)
 Section cross-reference(s): 9, 17, 63

FAN.CNT 2

	PATENT NO.	KIND	DATE	APPLICATION NO.	DATE
PI	US 6096870	A	20000801	US 1998-76169	19980504 <--
	US 5756680	A	19980526	US 1996-678364	19960716 <--
PRAI	US 1994-177574	B1	19940105 <--		
	US 1996-678364	A2	19960716 <--		

AB The present invention is related to the sepn. of whey proteins, particularly the sequential sepn. of whey proteins into sep. fractions through the use of chromatog. The present invention further provides methods and compns. for the sequential sepn. of whey proteins, as well as their use in various products. The present invention also provides methods and compns. for the cleaning of chromatog. resins used in the sepn. of whey proteins. The whey protein is selected from the group consisting of Ig. (e.g. IgG), .beta.-lactoglobulin, .alpha.-lactalbumin, lactoperoxidase, serum albumin, and lactoferrin; and the products is nutritional or supplements, feed constituent, and/or filler as well as food products such as sports drinks, fruit gels, ice cream, cookies, beverages, confectionery items, candies, convenience food, desserts, baked goods, sauces, infant foods and formulas, geriatric foods, animal feeds and as drug constituent.

ST whey protein chromatog sepn nutrient supplement

- IT Immunoglobulins
 - RL: BUU (Biological use, unclassified); FFD (Food or feed use); PUR (Purification or recovery); THU (Therapeutic use); BIOL (Biological study); PREP (Preparation); USES (Uses)
 - (G; chromatog. sepn. of whey proteins for use in food, nutritional and supplements, feed and drug products)
- IT Whey
 - (acid, pasteurized; chromatog. sepn. of whey proteins for use in food, nutritional and supplements, feed and drug products)
- IT Flow
 - (axial, chromatog. column; chromatog. sepn. of whey proteins for use in food, nutritional and supplements, feed and drug products)
- IT Polymers, biological studies
 - RL: BUU (Biological use, unclassified); DEV (Device component use); BIOL (Biological study); USES (Uses)
 - (carboxymethyl or dithylaminoethyl; chromatog. sepn. of whey proteins for use in food, nutritional and supplements, feed and drug products)
- IT Containers
 - (chamber; chromatog. sepn. of whey proteins for use in food, nutritional and supplements, feed and drug products)
- IT Anion exchangers
 - Bakery products
 - Beverages
 - Buffers
 - Candy
 - Cation exchangers
 - Chromatography
 - Confectionery
 - Containers
 - Desserts
 - Emulsifying agents
 - Feed
 - Fillers
 - Freeze drying
 - Ice cream
 - Nutrients
 - Sauces (condiments)
 - Tanks (containers)
 - Ultrafilters
 - (chromatog. sepn. of whey proteins for use in food, nutritional and supplements, feed and drug products)

- IT Minerals, biological studies
- Vitamins
 - RL: BUU (Biological use, unclassified); BIOL (Biological study); USES (Uses)
 - (chromatog. sepn. of whey proteins for use in food, nutritional and supplements, feed and drug products)
- IT Immunoglobulins
- Lactoferrins
- Lipoproteins
 - RL: BUU (Biological use, unclassified); FFD (Food or feed use); PUR (Purification or recovery); THU (Therapeutic use); BIOL (Biological study); PREP (Preparation); USES (Uses)
 - (chromatog. sepn. of whey proteins for use in food, nutritional and supplements, feed and drug products)
- IT Drugs
- Health products
 - (constituents; chromatog. sepn. of whey proteins for use in food, nutritional and supplements, feed and drug products)
- IT Bakery products
- (cookies; chromatog. sepn. of whey proteins for use in food, nutritional and supplements, feed and drug products)
- IT Sponges (artificial)

(crosslinked flexible absorbent; chromatog. sepn. of whey proteins for use in food, nutritional and supplements, feed and drug products)

IT Absorbents
(crosslinked flexible sponge; chromatog. sepn. of whey proteins for use in food, nutritional and supplements, feed and drug products)

IT Containers
(cups; chromatog. sepn. of whey proteins for use in food, nutritional and supplements, feed and drug products)

IT Aging, animal
(food; chromatog. sepn. of whey proteins for use in food, nutritional and supplements, feed and drug products)

IT Food gels
(fruit; chromatog. sepn. of whey proteins for use in food, nutritional and supplements, feed and drug products)

IT Fruit
(gels; chromatog. sepn. of whey proteins for use in food, nutritional and supplements, feed and drug products)

IT Milk substitutes
(human, non-allergic; chromatog. sepn. of whey proteins for use in food, nutritional and supplements, feed and drug products)

IT Food
(infant, non-allergic; chromatog. sepn. of whey proteins for use in food, nutritional and supplements, feed and drug products)

IT Whey
(pasteurized; chromatog. sepn. of whey proteins for use in food, nutritional and supplements, feed and drug products)

IT Flow
(radial flow, chromatog. column; chromatog. sepn. of whey proteins for use in food, nutritional and supplements, feed and drug products)

IT Liquid chromatography
(radial or axial; chromatog. sepn. of whey proteins for use in food, nutritional and supplements, feed and drug products)

IT Proteins, general, biological studies
RL: BUU (Biological use, unclassified); FFD (Food or feed use); PUR (Purification or recovery); THU (Therapeutic use); BIOL (Biological study); PREP (Preparation); USES (Uses)
(sepn.; chromatog. sepn. of whey proteins for use in food, nutritional and supplements, feed and drug products)

IT Albumins, biological studies
RL: BUU (Biological use, unclassified); FFD (Food or feed use); PUR (Purification or recovery); THU (Therapeutic use); BIOL (Biological study); PREP (Preparation); USES (Uses)
(serum; chromatog. sepn. of whey proteins for use in food, nutritional and supplements, feed and drug products)

IT Beverages
(sports; chromatog. sepn. of whey proteins for use in food, nutritional and supplements, feed and drug products)

IT Drying
(spray; chromatog. sepn. of whey proteins for use in food, nutritional and supplements, feed and drug products)

IT Food
(supplement; chromatog. sepn. of whey proteins for use in food, nutritional and supplements, feed and drug products)

IT Containers
(vat; chromatog. sepn. of whey proteins for use in food, nutritional and supplements, feed and drug products)

IT Proteins, specific or class
RL: BUU (Biological use, unclassified); FFD (Food or feed use); PUR (Purification or recovery); THU (Therapeutic use); BIOL (Biological study); PREP (Preparation); USES (Uses)
(whey; chromatog. sepn. of whey proteins for use in food, nutritional and supplements, feed and drug products)

IT Lactalbumins

RL: BUU (Biological use, unclassified); FFD (Food or feed use); PUR (Purification or recovery); THU (Therapeutic use); BIOL (Biological study); PREP (Preparation); USES (Uses)

(.alpha.-; chromatog. sepn. of whey proteins for use in food, nutritional and supplements, feed and drug products)

IT Lactoglobulins

RL: BUU (Biological use, unclassified); FFD (Food or feed use); PUR (Purification or recovery); THU (Therapeutic use); BIOL (Biological study); PREP (Preparation); USES (Uses)

(.beta.-; chromatog. sepn. of whey proteins for use in food, nutritional and supplements, feed and drug products)

IT 50-21-5, Lactic acid, biological studies 63-42-3, Lactose 64-17-5, Ethanol, biological studies 127-09-3, Sodium acetate 994-36-5, Sodium citrate 1310-73-2, Sodium hydroxide, biological studies 7647-01-0, Hydrochloric acid, biological studies 7647-14-5, Sodium chloride, biological studies 7681-52-9, Sodium hypochlorite

RL: BUU (Biological use, unclassified); BIOL (Biological study); USES (Uses)

(chromatog. sepn. of whey proteins for use in food, nutritional and supplements, feed and drug products)

IT 106-91-2D, Glycidyl methacrylate, **copolymers** 111-46-6D, Diethylene glycol, crosslinked 136218-99-0, Macro-Prep 50S 140876-37-5, Macro-Prep 50Q 188039-62-5, Macro-Prep High S 203210-61-1, Macro-Prep HQ 287118-15-4, SepraSorb CM 287118-16-5, SepraSorb DE

RL: BUU (Biological use, unclassified); DEV (Device component use); BIOL (Biological study); USES (Uses)

(chromatog. sepn. of whey proteins for use in food, nutritional and supplements, feed and drug products)

IT 9003-99-0P, Lactoperoxidase

RL: BUU (Biological use, unclassified); FFD (Food or feed use); PUR (Purification or recovery); THU (Therapeutic use); BIOL (Biological study); PREP (Preparation); USES (Uses)

(chromatog. sepn. of whey proteins for use in food, nutritional and supplements, feed and drug products)

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 IT 7647-01-0, Hydrochloric acid, biological studies 7647-14-5
 , Sodium chloride, biological studies
 RL: BUU (Biological use, unclassified); BIOL (Biological study); USES
 (Uses)
 (chromatog. sepn. of whey proteins for use in food, nutritional and
 supplements, feed and drug products)
 RN 7647-01-0 HCAPLUS
 CN Hydrochloric acid (6CI, 7CI, 8CI, 9CI) (CA INDEX NAME)

HCl

RN 7647-14-5 HCAPLUS
 CN Sodium chloride (NaCl) (9CI) (CA INDEX NAME)

Cl-Na

L86 ANSWER 2 OF 21 HCAPLUS COPYRIGHT 2003 ACS
 AN 2000:129194 HCAPLUS
 DN 132:276538
 TI A folding variant of .alpha.-lactalbumin with
 bactericidal activity against Streptococcus pneumoniae
 AU Hakansson, Anders; Svensson, Malin; Mossberg,
 Ann-Kristin; Sabharwal, Hemant; Linse, Sara; Lazou, Irene; Lonnerdal, Bo;
 Svanborg, Catharina
 CS Department of Microbiology, Immunology and Glycobiology, Institute of
 Laboratory Medicine, Lund University, Lund, SE-223 62, Swed.
 SO Molecular Microbiology (2000), 35(3), 589-600
 CODEN: MOMIEE; ISSN: 0950-382X
 PB Blackwell Science Ltd.
 DT Journal
 LA English

bad date

CC 10-5 (Microbial, Algal, and Fungal Biochemistry)
AB This study describes an *.alpha.-lactalbumin* folding variant from human milk with bactericidal activity against antibiotic-resistant and -susceptible strains of *Streptococcus pneumoniae*. The active complex pptd. with the casein fraction at pH 4.6 and was purified from casein by a combination of anion exchange and gel chromatog. Unlike other casein components, the active complex was retained on the ion-exchange matrix and eluted only with high salt. The eluted fraction showed N-terminal and mass spectrometric identity with human milk *.alpha.-lactalbumin*, but native *.alpha.-lactalbumin* had no bactericidal effect. Spectroscopic anal. demonstrated that the active form of the mol. was in a different folding state, with secondary structure identical to *.alpha.-lactalbumin* from human milk whey, but fluctuating tertiary structure. Native *.alpha.-lactalbumin* could be converted to the active bactericidal form by ion-exchange chromatog. in the presence of a cofactor from human milk casein, characterized as a C18:1 fatty acid. Anal. of the antibacterial spectrum showed selectivity for streptococci; Gram-neg. and other Gram-pos. bacteria were resistant. The folding variant of *.alpha.-lactalbumin* is a new example of naturally occurring mols. with antimicrobial activity.

ST *lactalbumin* antibacterial *Streptococcus*

IT Antibacterial agents

Streptococcus pneumoniae

(folding variant of *.alpha.-lactalbumin* from human milk with bactericidal activity against *Streptococcus pneumoniae*)

IT Milk

(human; folding variant of *.alpha.-lactalbumin* from human milk with bactericidal activity against *Streptococcus pneumoniae*)

IT *Lactalbumins*

RL: BAC (Biological activity or effector, except adverse); BSU (Biological study, unclassified); PRP (Properties); PUR (Purification or recovery); BIOL (Biological study); PREP (Preparation)
(*.alpha.-*; folding variant of *.alpha.-lactalbumin* from human milk with bactericidal activity against *Streptococcus pneumoniae*)

RE.CNT 50 THERE ARE 50 CITED REFERENCES AVAILABLE FOR THIS RECORD

RE

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L86 ANSWER 3 OF 21 HCAPLUS COPYRIGHT 2003 ACS

AN 1999:733053 HCAPLUS

DN 131:334330

TI Isolating .beta.-lactoglobulin and .alpha.-lactalbumin by eluting from a cation exchanger without sodium chloride

IN Etzel, Mark R.

PA Wisconsin Alumni Research Foundation, USA

SO U.S., 16 pp.

CODEN: USXXAM

DT Patent

LA English

IC ICM C07K001-18

ICS C07K014-435; A23J001-20

NCL 530366000

CC 9-3 (Biochemical Methods)

Section cross-reference(s): 13

FAN.CNT 1

	PATENT NO.	KIND	DATE	APPLICATION NO.	DATE
PI	US 5986063	A	19991116	US 1998-126904	19980731 <--
PRAI	US 1998-126904		19980731 <--		
AB	A method is provided for isolating the proteins, .beta.-lactoglobulin and .alpha.-lactalbumin, from whey with a single cation exchanger, and using different pH values for eluting the proteins as sep. fractions without using salt elution. A whey protein soln. is adjusted to a pH of less than about 4.5. The soln. is contacted with a cation exchanger to obtain a bound fraction contg. .alpha.-lactalbumin and .beta.-lactoglobulin. The bound fraction is adjusted to a pH of about 4.0 to 6.0 and a .beta.-lactoglobulin fraction is eluted at this pH in the absence of sodium chloride. The pH of an remaining bound fraction is adjusted to about 6.5 or greater and an .alpha.-lactalbumin fraction is eluted. The method is advantageously conducted at elevated temps. ranging from 35.degree. C. to 50.degree. C. The ion exchanger may be cross-linked polymeric beads made of cellulose, agarose or dextran, or a microporous				

polymeric membrane made of regenerated cellulose, polysulfone or cellulose acetate, and may contain charged immobilized mols. such as carboxymethyl or sulfopropyl moieties.

ST whey lactoglobulin **lactalbumin** cation exchange chromatog pH

IT Membranes, nonbiological
(porous, contg. charged immobilized groups, as cation exchanger; .beta.-lactoglobulin and .alpha.-lactalbumin
isolation from whey by eluting from cation exchanger without sodium chloride)

IT Proteins, specific or class
RL: PEP (Physical, engineering or chemical process); PROC (Process)
(whey; .beta.-lactoglobulin and .alpha.-lactalbumin
isolation from whey by eluting from cation exchanger without sodium chloride)

IT Lactalbumins
RL: PUR (Purification or recovery); PREP (Preparation)
(.alpha.-; .beta.-lactoglobulin and .alpha.-
lactalbumin isolation from whey by eluting from cation exchanger without sodium chloride)

IT Lactoglobulins
RL: PUR (Purification or recovery); PREP (Preparation)
(.beta.-; .beta.-lactoglobulin and .alpha.-
lactalbumin isolation from whey by eluting from cation exchanger without sodium chloride)

IT Cation exchange chromatography
Cation exchangers
Whey
pH
(.beta.-lactoglobulin and .alpha.-lactalbumin
isolation from whey by eluting from cation exchanger without sodium chloride)

IT 71-00-1, L-Histidine, uses 7786-30-3, Magnesium chloride, uses 10043-52-4, Calcium chloride, uses
RL: NUU (Other use, unclassified); USES (Uses)
(in .alpha.-lactalbumin desorption;
.beta.-lactoglobulin and .alpha.-lactalbumin
isolation from whey by eluting from cation exchanger without sodium chloride)

IT 7647-14-5, Sodium chloride, miscellaneous
RL: MSC (Miscellaneous)
(.beta.-lactoglobulin and .alpha.-lactalbumin
isolation from whey by eluting from cation exchanger without sodium chloride)

RE.CNT 1 THERE ARE 1 CITED REFERENCES AVAILABLE FOR THIS RECORD

RE
(1) Uchida; US 5516675 1996 HCPLUS

IT 7647-14-5, Sodium chloride, miscellaneous
RL: MSC (Miscellaneous)
(.beta.-lactoglobulin and .alpha.-lactalbumin
isolation from whey by eluting from cation exchanger without sodium chloride)

RN 7647-14-5 HCPLUS

CN Sodium chloride (NaCl) (9CI) (CA INDEX NAME)

Cl-Na

L86 ANSWER 4 OF 21 HCPLUS COPYRIGHT 2003 ACS
 AN 1999:355804 HCPLUS
 DN 131:23495
 TI Ion exchange chromatography for preparation

of .alpha.-lactalbumin

IN Svanborg, Catharina; Svensson, Malin Wilhelmina;
Hakansson, Per Anders

PA Swed.

SO PCT Int. Appl., 49 pp.
CODEN: PIXXD2

DT Patent

LA English

IC ICM C07K014-76

ICS A61K038-38; B01D015-08

CC 63-3 (Pharmaceuticals)

Section cross-reference(s): 1

FAN.CNT 1

	PATENT NO.	KIND	DATE	APPLICATION NO.	DATE
PI	WO 9926979	A1	19990603	WO 1998-IB1919	19981123 <-- W: AL, AM, AT, AU, AZ, BA, BB, BG, BR, BY, CA, CH, CN, CU, CZ, DE, DK, EE, FI, GB, GE, GH, GM, HR, HU, ID, IL, IS, JP, KE, KG, KP, KR, KZ, LC, LK, LS, LT, LU, LV, MD, MG, MK, MN, MW, MX, NO, NZ, PL, PT, RO, RU, SD, SE, SG, SI, SK, SL, TJ, TM, TR, TT, UA, UG, US, UZ, VN, YU, ZW, AM, AZ, BY, KG, KZ, MD, RU, TJ, TM RW: GH, GM, KE, LS, MW, SD, SZ, UG, ZW, AT, BE, CH, CY, DE, DK, ES, FI, FR, GB, GR, IE, IT, LU, MC, NL, PT, SE, BF, BJ, CF, CG, CI, CM, GA, GN, GW, ML, MR, NE, SN, TD, TG
	AU 9912541	A1	19990615	AU 1999-12541	19981123 <--
	EP 1032596	A1	20000906	EP 1998-955823	19981123 <-- R: AT, BE, CH, DE, DK, ES, FR, GB, GR, IT, LI, LU, NL, SE, MC, PT, IE, FI
	JP 2001524491	T2	20011204	JP 2000-522135	19981123 <--
PRAI	GB 1997-24725	A	19971121	<--	
	GB 1998-12202	A	19980605	<--	
	WO 1998-IB1919	W	19981123	<--	

AB An ion exchange method for prepn. of an **oligomeric** form of .
.alpha.-lactalbumin comprises exposing a source of .
.alpha.-lactalbumin, in which the .alpha.-
lactalbumin is preferably in the **globule-like** state, to
an ion exchange medium which has been pretreated with casein or an active
component thereof, such as oleic acid, and recovering .alpha.-
lactalbumin in an **oligomeric** form therefrom.
Pretreatment of the ion exchange medium, particularly with casein derived
from human milk, has been found to significantly improve yields of the
oligomeric form of .alpha.-lactalbumin and
mean that it can readily isolated from readily available sources such as
bovine .alpha.-lactalbumin. This form of .
.alpha.-lactalbumin is useful therapeutically, in
particular as an antibacterial agent and also as an anticancer
therapeutic. The occurrence of DNA fragmentation, indicative of
apoptosis, was obsd. when tumor cells were treated with **multimeric**
.alpha.-lactalbumin prep'd. by using a DEAE-trisacryl M
ion exchange column.

ST milk lactalbumin ion exchange antibacterial anticancer

IT Liquid chromatographic stationary phases

Liquid chromatographic stationary phases
(anion exchange; ion exchange
chromatog. for prepn. of .alpha.-lactalbumin
for therapeutic uses)

IT Chelating agents

(calcium; ion exchange chromatog. for
prep. of .alpha.-lactalbumin for therapeutic uses)

IT Fatty acids, uses

Lipids, uses

RL: MOA (Modifier or additive use); USES (Uses)
(casein; ion exchange chromatog. for

End date

prepn. of .alpha.-lactalbumin for therapeutic uses)

IT Milk
Milk
(frozen; ion exchange chromatog. for
prepn. of .alpha.-lactalbumin for therapeutic uses)

IT Antibacterial agents
Antitumor agents
Ion exchange
Ion exchange liquid chromatography
Milk
(ion exchange chromatog. for prepn. of
.alpha.-lactalbumin for therapeutic uses)

IT Caseins, uses
RL: MOA (Modifier or additive use); USES (Uses)
(ion exchange chromatog. for prepn. of
.alpha.-lactalbumin for therapeutic uses)

IT Frozen foods
Frozen foods
(milk; ion exchange chromatog. for prepn.
of .alpha.-lactalbumin for therapeutic uses)

IT Anion exchange liquid chromatography
Anion exchange liquid chromatography
(stationary phases; ion exchange chromatog
. for prepn. of .alpha.-lactalbumin for therapeutic
uses)

IT Lactalbumins
RL: BAC (Biological activity or effector, except adverse); BSU (Biological
study, unclassified); PUR (Purification or recovery); THU (Therapeutic
use); BIOL (Biological study); PREP (Preparation); USES (Uses)
.alpha.-; ion exchange chromatog
. for prepn. of .alpha.-lactalbumin for therapeutic
uses)

IT 1185-53-1, TRIS hydrochloride
RL: PRP (Properties)
(buffer contg.; ion exchange chromatog.
for prepn. of .alpha.-lactalbumin for therapeutic
uses)

IT 80701-61-7, DEAE-trisacryl M
RL: ARU (Analytical role, unclassified); ANST (Analytical study)
(column; ion exchange chromatog. for
prepn. of .alpha.-lactalbumin for therapeutic uses)

IT 60-00-4, EDTA, uses 112-80-1, 9-Octadecenoic acid (9Z)-,
uses 7647-01-0, Hydrochloric acid, uses 7647-14-5,
Sodium chloride, uses
RL: MOA (Modifier or additive use); USES (Uses)
(ion exchange chromatog. for prepn. of
.alpha.-lactalbumin for therapeutic uses)

RE.CNT 3 THERE ARE 3 CITED REFERENCES AVAILABLE FOR THIS RECORD

RE

(1) Jegouic, M; Journal of Agricultural and Food Chemistry 1997, V45(1), P19
HCAPLUS

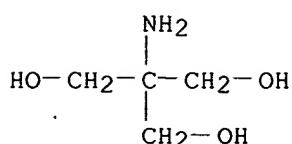
(2) Sabharwal & Svanborg; WO 9604929 A 1996 HCAPLUS

(3) Snow Brand Milk Products; FR 2671697 A 1992 HCAPLUS

IT 1185-53-1, TRIS hydrochloride
RL: PRP (Properties)
(buffer contg.; ion exchange chromatog.
for prepn. of .alpha.-lactalbumin for therapeutic
uses)

RN 1185-53-1 HCAPLUS

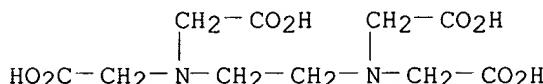
CN 1,3-Propanediol, 2-amino-2-(hydroxymethyl)-, hydrochloride (8CI, 9CI) (CA
INDEX NAME)



● HCl

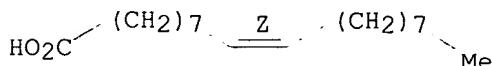
IT 80701-61-7, DEAE-trisacryl M
 RL: ARU (Analytical role, unclassified); ANST (Analytical study)
 (column; ion exchange chromatog. for
 prepn. of α -lactalbumin for therapeutic uses)
 RN 80701-61-7 HCPLUS
 CN Trisacryl M-DEAE (9CI) (CA INDEX NAME)

*** STRUCTURE DIAGRAM IS NOT AVAILABLE ***
 IT 60-00-4, EDTA, uses 112-80-1, 9-Octadecenoic acid (9Z)-,
 uses 7647-01-0, Hydrochloric acid, uses 7647-14-5,
 Sodium chloride, uses
 RL: MOA (Modifier or additive use); USES (Uses)
 (ion exchange chromatog. for prepn. of
 α -lactalbumin for therapeutic uses)
 RN 60-00-4 HCPLUS
 CN Glycine, N,N'-1,2-ethanediylbis[N-(carboxymethyl)- (9CI) (CA INDEX NAME)



RN 112-80-1 HCPLUS
 CN 9-Octadecenoic acid (9Z)- (9CI) (CA INDEX NAME)

Double bond geometry as shown.



RN 7647-01-0 HCPLUS
 CN Hydrochloric acid (6CI, 7CI, 8CI, 9CI) (CA INDEX NAME)

HCl

RN 7647-14-5 HCPLUS
 CN Sodium chloride (NaCl) (9CI) (CA INDEX NAME)

Cl-Na

L86 ANSWER 5 OF 21 HCPLUS COPYRIGHT 2003 ACS
 AN 1999:231486 HCPLUS
 DN 130:266618
 TI Sequential separation of whey proteins by radial-flow chromatography and

IN use of proteins in infant formula
 Ahmed, Salah H.; Saxena, Vinit; Miranda, Quirinus
 PA Sepragen Corporation, USA
 SO PCT Int. Appl., 37 pp.
 CODEN: PIXXD2

DT Patent
 LA English

IC ICM A23C009-14
 CC 17-8 (Food and Feed Chemistry)

FAN.CNT 1

	PATENT NO.	KIND	DATE	APPLICATION NO.	DATE
PI	WO 9915024	A1	19990401	WO 1997-US16993	19970922 <--
	W: AU, CA, JP, KR, NZ			RW: AT, BE, CH, DE, DK, ES, FI, FR, GB, GR, IE, IT, LU, MC, NL, PT, SE	
	AU 9745893	A1	19990412	AU 1997-45893	19970922 <--
	EP 1017286	A1	20000712	EP 1997-944384	19970922 <--
	R: AT, BE, CH, DE, DK, ES, FR, GB, GR, IT, LI, LU, NL, SE, MC, PT, IE, FI			JP 20001516599	T2 20011002 JP 2000-512418 19970922 <--
	JP 20001516599	T2	20011002	JP 2000-512418	19970922 <--
	NZ 503566	A	20021025	NZ 1997-503566	19970922 <--
PRAI	WO 1997-US16993	A	19970922 <--		

AB Buffer systems adjusted to suitable pH and ionic strength are utilized for sequential sepn. of whey proteins by radial-flow chromatog. The method permits sepn. of Ig, .beta.-lactoglobulin, .alpha.-lactalbumin, bovine serum albumin, and lactoferrin. Infant feeding formulas, and other food formulations may incorporate the various proteins sepd. from the whey. Thus, whey from mozzarella cheese manuf. is clarified, pasteurized, and the pH is adjusted to 3.8 for radial flow chromatog. on a column prepacked with a strong S cation exchange resin. Nonprotein constituents pass through the column, and the protein fractions are sequentially eluted.

ST whey protein radial flow chromatog

IT Milk substitutes

(human; sequential sepn. of whey proteins by radial-flow chromatog. and use of proteins in infant formula)

IT Caseins, biological studies

RL: FFD (Food or feed use); BIOL (Biological study); USES (Uses)
 (hydrolyzates; sequential sepn. of whey proteins by radial-flow chromatog. and use of proteins in infant formula)

IT Liquid chromatography

(radial-flow; sequential sepn. of whey proteins by radial-flow chromatog. and use of proteins in infant formula)

IT Proteins, general, preparation

RL: PUR (Purification or recovery); PREP (Preparation)
 (sepn.; sequential sepn. of whey proteins by radial-flow chromatog. and use of proteins in infant formula)

IT Cation exchangers

Sweetening agents

Ultrafiltration

Whey

(sequential sepn. of whey proteins by radial-flow chromatog. and use of proteins in infant formula)

IT Carbohydrates, biological studies

Fat substitutes

Mineral elements, biological studies

Vitamins

RL: FFD (Food or feed use); BIOL (Biological study); USES (Uses)
 (sequential sepn. of whey proteins by radial-flow chromatog. and use of proteins in infant formula)

IT Immunoglobulins

Lactoferrins

RL: FFD (Food or feed use); PUR (Purification or recovery); BIOL

(Biological study); PREP (Preparation); USES (Uses)
 (sequential sepn. of whey proteins by radial-flow chromatog. and use of
 proteins in infant formula)

IT Albumins, biological studies
 RL: FFD (Food or feed use); PUR (Purification or recovery); BIOL
 (Biological study); PREP (Preparation); USES (Uses)
 (serum; sequential sepn. of whey proteins by radial-flow chromatog. and
 use of proteins in infant formula)

IT Milk
 (solids; sequential sepn. of whey proteins by radial-flow chromatog.
 and use of proteins in infant formula)

IT Proteins, specific or class
 RL: FFD (Food or feed use); PEP (Physical, engineering or chemical
 process); BIOL (Biological study); PROC (Process); USES (Uses)
 (whey; sequential sepn. of whey proteins by radial-flow chromatog. and
 use of proteins in infant formula)

IT Lactalbumins
 RL: FFD (Food or feed use); PUR (Purification or recovery); BIOL
 (Biological study); PREP (Preparation); USES (Uses)
 (.alpha.-; sequential sepn. of whey proteins by radial-flow
 chromatog. and use of proteins in infant formula)

IT Lactoglobulins
 RL: FFD (Food or feed use); PUR (Purification or recovery); BIOL
 (Biological study); PREP (Preparation); USES (Uses)
 (.beta.-; sequential sepn. of whey proteins by radial-flow chromatog.
 and use of proteins in infant formula)

RE.CNT 4 THERE ARE 4 CITED REFERENCES AVAILABLE FOR THIS RECORD

RE

- (1) Harju; US 4820348 A 1989 HCPLUS
- (2) Lauer; US 3969337 A 1976 HCPLUS
- (3) Moeller; US 5085881 A 1992
- (4) Thibault; US 5077067 A 1991 HCPLUS

L86 ANSWER 6 OF 21 HCPLUS COPYRIGHT 2003 ACS
 AN 1998:699847 HCPLUS
 DN 130:80601
 TI Rapid separation of bovine whey proteins by membrane convective liquid chromatography, perfusion chromatography, continuous bed chromatography, and capillary electrophoresis
 AU Girardet, Jean-Michel; Saulnier, Franck; Linden, Guy; Humbert, Gerard
 CS Laboratoire des biosciences de l'aliment, unite associee a l'Inra, Faculte des sciences, universite Henri-Poincare Nancy I, Vandoeuvre-les-Nancy, 54506, Fr.
 SO Lait (1998), 78(4), 391-400
 CODEN: LAITAG; ISSN: 0023-7302
 PB Editions Scientifiques et Medicales Elsevier *had date*
 DT Journal
 LA English
 CC 17-6 (Food and Feed Chemistry)
 AB Membrane convective liq. chromatog. is a technique based on porous cellulose membranes designed for the sepn. of biomols. in few minutes at high flow-rates and low back-pressures. Bovine whey proteins are sepd. in less than 10 min, at pH 8.5, with a flow-rate of 5.6 mL/min and with a 0-0.2 mol/L NaCl linear gradient. Three other rapid methods are also proposed. With the ion-exchange perfusion liq. chromatog. based on beads with large pores and with the continuous bed chromatog. based on a polymer matrix, sepn. are achieved in only 10 min. Capillary zone electrophoresis using an untreated fused-silica capillary allows the sepn. of whey proteins in a single run of 8 min without the presence of polymeric additives. These rapid methods are suitable in the quality control of wheys and could be applied in the dairy industry or in research.
 ST whey protein sepn liq chromatog electrophoresis

IT Chromatography
 (continuous bed; rapid sepn. of bovine whey proteins by membrane convective liq. chromatog., perfusion chromatog., continuous bed chromatog., and capillary electrophoresis)

IT Capillary electrophoresis
 Liquid chromatography
 (rapid sepn. of bovine whey proteins by membrane convective liq. chromatog., perfusion chromatog., continuous bed chromatog., and capillary electrophoresis)

IT Albumins, preparation
 RL: PEP (Physical, engineering or chemical process); PUR (Purification or recovery); PREP (Preparation); PROC (Process)
 (serum; rapid sepn. of bovine whey proteins by membrane convective liq. chromatog., perfusion chromatog., continuous bed chromatog., and capillary electrophoresis)

IT Proteins, specific or class
 RL: PEP (Physical, engineering or chemical process); PUR (Purification or recovery); PREP (Preparation); PROC (Process)
 (whey; rapid sepn. of bovine whey proteins by membrane convective liq. chromatog., perfusion chromatog., continuous bed chromatog., and capillary electrophoresis)

IT Lactalbumins
 RL: PEP (Physical, engineering or chemical process); PUR (Purification or recovery); PREP (Preparation); PROC (Process)
 (.alpha.-; rapid sepn. of bovine whey proteins by membrane convective liq. chromatog., perfusion chromatog., continuous bed chromatog., and capillary electrophoresis)

IT Lactoglobulins
 RL: PEP (Physical, engineering or chemical process); PUR (Purification or recovery); PREP (Preparation); PROC (Process)
 (.beta.-, A; rapid sepn. of bovine whey proteins by membrane convective liq. chromatog., perfusion chromatog., continuous bed chromatog., and capillary electrophoresis)

IT Lactoglobulins
 RL: PEP (Physical, engineering or chemical process); PUR (Purification or recovery); PREP (Preparation); PROC (Process)
 (.beta.-, B; rapid sepn. of bovine whey proteins by membrane convective liq. chromatog., perfusion chromatog., continuous bed chromatog., and capillary electrophoresis)

RE.CNT 17 THERE ARE 17 CITED REFERENCES AVAILABLE FOR THIS RECORD

RE

- (1) Afeyan, N; J Chromatogr 1990, V519, P1 HCPLUS
- (2) Andrews, A; J Chromatogr 1985, V348, P177 HCPLUS
- (3) Cifuentes, A; J Dairy Sci 1993, V76, P1870 HCPLUS
- (4) Gerstner, J; J Chromatogr 1992, V596, P173 HCPLUS
- (5) Girardet, J; Milchwissenschaft 1989, V44, P692 HCPLUS
- (6) Hjerten, S; J Chromatogr 1989, V473, P273 HCPLUS
- (7) Lindeberg, J; Food Chem 1996, V55, P73 HCPLUS
- (8) Musci, G; Biochemistry 1985, V24, P3852 HCPLUS
- (9) Otte, J; Neth Milk Dairy J 1994, V48, P81 HCPLUS
- (10) Recio, I; Electrophoresis 1995, V16, P654 HCPLUS
- (11) Ribadeau, D; Lait 1991, V71, P133
- (12) Splitt, H; J Chromatogr 1996, V729, P87 HCPLUS
- (13) Strange, E; J Chromatogr 1992, V624, P81 HCPLUS
- (14) Torre, M; J Chromatogr 1996, V729, P99 HCPLUS
- (15) van Deemter, J; Chem Eng Sci 1956, V5, P271 HCPLUS
- (16) Watzig, H; Pharmazie 1994, V49, P83 MEDLINE
- (17) Weinbrenner, W; J Chromatogr 1994, V662, P414 HCPLUS

L86 ANSWER 7 OF 21 HCPLUS COPYRIGHT 2003 ACS

AN 1998:590212 HCPLUS

DN 129:313776

TI Samples of human .alpha.-lactalbumin, inducing

AU apoptosis of transformed cells, containing ribooligonucleotides
AU Kit, Yu. Ya.; Kuligina, E. V.; Romannikova, I. V.; Semenov, D. V.;
AU Rikhter, V. A.; Vlasov, V. V.
CS Novosibirsk. Inst. Bioorg. Khim., Sib. Otd. Ross. Akad. Nauk, Novosibirsk,
Russia
SO Doklady Akademii Nauk (1998), 360(3), 406-408
CODEN: DAKNEQ; ISSN: 0869-5652
PB MAIK Nauka
DT Journal
LA Russian
CC 13-1 (Mammalian Biochemistry)
Section cross-reference(s): 6, 18
AB Oligonucleotides of different sizes were found in samples of human .alpha.-lactalbumin "Sigma" and in human milk caseins contg. .alpha.-lactalbumin. Large oligonucleotides can be hydrolyzed by RNAase A and sepd. from .alpha.-lactalbumin by ion-exchange chromatog. The influence of the oligonucleotides on the formation of multimeric forms of .alpha.-lactalbumin and on cytotoxic activity of human milk is discussed.
ST alpha lactalbumin oligonucleotide casein
human milk
IT Milk
(human; samples of human .alpha.-lactalbumin, inducing apoptosis of transformed cells, contg. ribooligonucleotides)
IT Oligonucleotides
RL: BOC (Biological occurrence); BPR (Biological process); BSU (Biological study, unclassified); PUR (Purification or recovery); BIOL (Biological study); OCCU (Occurrence); PREP (Preparation); PROC (Process)
(samples of human .alpha.-lactalbumin, inducing apoptosis of transformed cells, contg. ribooligonucleotides)
IT Caseins, properties
RL: PRP (Properties)
(samples of human .alpha.-lactalbumin, inducing apoptosis of transformed cells, contg. ribooligonucleotides)
IT Lactalbumins
RL: BPR (Biological process); BSU (Biological study, unclassified); PRP (Properties); PUR (Purification or recovery); BIOL (Biological study); PREP (Preparation); PROC (Process)
(.alpha.-; samples of human .alpha.-lactalbumin, inducing apoptosis of transformed cells, contg. ribooligonucleotides)

L86 ANSWER 8 OF 21 HCPLUS COPYRIGHT 2003 ACS
AN 1998:585149 HCPLUS
DN 129:342863
TI Extraction of .alpha.-lactalbumin from whey protein concentrate with modified inorganic membranes
AU Lucas, David; Rabiller-Baudry, Murielle; Millesime, Luc; Chaufer, Bernard; Daufin, Georges
CS Laboratoire des Procedes de Separation, UA Universite de Rennes 1-INRA, Rennes, 35000, Fr.
SO Journal of Membrane Science (1998), 148(1), 1-12
CODEN: JAMESDO; ISSN: 0376-7388
PB Elsevier Science B.V.
DT Journal
LA English
CC 17-8 (Food and Feed Chemistry)
AB A study was made to ext. .alpha.-lactalbumin (.alpha.-LA) selectively from acid casein whey protein conc. (WPC) at pH 7 by limiting .beta.-lactoglobulin (.beta.-LG) transmission. In order to achieve a high selectivity (ratio of .alpha.-LA

transmission/.beta.-LG transmission), inorg. membranes were chem. modified by a polyethyleneimine coating bearing pos. charges. In-depth study by anion-exchange chromatog. with a similar polymer coating suggests the possibility a more selective ion-exchange process with .beta.-LG by the membrane at low or moderate ionic strength. Accordingly, transmission was investigated vs. ionic strength (NaCl added): transmission of .beta.-lactoglobulin was lowered with the modified membrane (.alpha.-LA transmission about 10%) and selectivities close to 10, were achieved at low ionic strength ($I \leq 0.02 \text{ mol L}^{-1}$) when unmodified membrane selectivities were about 3 whatever the mol.-wt. cut-off. High selectivity of the tailor-made membrane was due to the adjustment of mol. sieving combined with anion-exchange interactions between neg. charged .beta.-LG and the membrane, the reversible fouling of which was enhanced. Modification of the net charge of protein by specific adsorption of divalent ion such as calcium or phosphate increased or decreased the transmission of protein, resp., but the membrane selectivity was similar because the adsorption of divalent ion occurred on the two proteins.

ST lactalbumin extn whey protein ultrafiltration membrane
 IT Anion exchange
 Fouling
 Ionic strength
 Ultrafiltration
 (extn. of .alpha.-lactalbumin from whey protein
 conc. by using modified inorg. membranes)
 IT Adsorption
 /ion; extn. of .alpha.-lactalbumin from whey
 protein conc. by using modified inorg. membranes)
 IT Ultrafilters
 (polyethyleneimine; extn. of .alpha.-lactalbumin
 from whey protein conc. by using modified inorg. membranes)
 IT Proteins, specific or class
 RL: FFD (Food or feed use); PEP (Physical, engineering or chemical
 process); BIOL (Biological study); PROC (Process); USES (Uses)
 (whey; extn. of .alpha.-lactalbumin from whey
 protein conc. by using modified inorg. membranes)
 IT Lactalbumins
 RL: FFD (Food or feed use); PUR (Purification or recovery); BIOL
 (Biological study); PREP (Preparation); USES (Uses)
 (.alpha.-; extn. of .alpha.-lactalbumin
 from whey protein conc. by using modified inorg. membranes)
 IT Lactoglobulins
 RL: FFD (Food or feed use); PEP (Physical, engineering or chemical
 process); BIOL (Biological study); PROC (Process); USES (Uses)
 (.beta.-; extn. of .alpha.-lactalbumin from whey
 protein conc. by using modified inorg. membranes)
 IT 7440-70-2, Calcium, processes 14265-44-2, Phosphate, processes
 RL: PEP (Physical, engineering or chemical process); PROC (Process)
 (adsorption; extn. of .alpha.-lactalbumin from whey
 protein conc. by using modified inorg. membranes)
 IT 9002-98-6
 RL: FFD (Food or feed use); BIOL (Biological study); USES (Uses)
 (membrane coating; extn. of .alpha.-lactalbumin
 from whey protein conc. by using modified inorg. membranes)
 IT 1314-23-4, Zirconium oxide, biological studies
 RL: FFD (Food or feed use); BIOL (Biological study); USES (Uses)
 (membrane; extn. of .alpha.-lactalbumin from whey
 protein conc. by using modified inorg. membranes)
 RE.CNT 26 THERE ARE 26 CITED REFERENCES AVAILABLE FOR THIS RECORD
 RE
 (1) Chaufer, B; J Chromatogr 1991, V548, P215 HCAPLUS
 (2) Chaufer, B; Key Eng Mater 1991, V61(62), P249

- (3) Chaufer, B; Unpublished results
- (4) Dumon, S; J Membr Sci 1992, V74, P289 HCAPLUS
- (5) Eigel, W; J Dairy Sci 1984, V67, P1599 HCAPLUS
- (6) Ingham, K; Polymer Science and Technology 1980, V13, P141 HCAPLUS
- (7) Ko, M; J Membr Sci 1993, V76, P101 HCAPLUS
- (8) Kopaciewicz, W; J Chromatogr 1983, V266, P3 HCAPLUS
- (9) Le Berre, O; J Membr Sci 1994, V88, P263 HCAPLUS
- (10) Lemque, R; J Chromatogr 1991, V553, P165 HCAPLUS
- (11) Lucas, D; Colloids Surf A 1998, V136, P109 HCAPLUS
- (12) Mehra, R; J Dairy Res 1993, V60, P89 HCAPLUS
- (13) Millesime, L; Bioseparation 1996, V6, P135 HCAPLUS
- (14) Millesime, L; J Membr Sci 1995, V108, P143 HCAPLUS
- (15) Millesime, L; Langmuir 1996, V12, P3377 HCAPLUS
- (16) Muller, A; Ph D Thesis, Ecole Nationale Supérieure Agronomique 1996
- (17) Nakao, S; Desalination 1988, V70, P191 HCAPLUS
- (18) Patocka, G; Can Inst Sci Technol J 1991, V24, P218
- (19) Peters, T; Serum Albumin in Advances in Protein Chemistry 1985, P161 HCAPLUS
- (20) Rabiller-Baudry, M; J Chromatogr B 1998, V706, P23 HCAPLUS
- (21) Randon, J; Colloids Surf A 1991, V52, P241 HCAPLUS
- (22) Resmini, P; Sci E Technica Latterio-Casearia 1989, V40, P7
- (23) Ricq, L; Ph D Thesis, Université de Franche-Comté 1996
- (24) Saksena, S; Biotechnol Bioeng 1994, V43, P860
- (25) Swaisgood, H; Developments in Dairy Chemistry, Chapter 1 1982
- (26) Zhang, L; Desalination 1993, V90, P137 HCAPLUS

L86 ANSWER 9 OF 21 HCAPLUS COPYRIGHT 2003 ACS

AN 1998:392096 HCAPLUS

DN 129:25387

TI Sequential separation of whey proteins and formulations thereof

IN Ahmed, Salah H.; Saxena, Vinit; Mozaffar, Zahid; Miranda, Quirinus R.

PA Sepragen Corp., USA

SO U.S., 13 pp., Cont. of U. S. Ser. No. 177,574, abandoned.

CODEN: USXXAM

DT Patent

LA English

IC ICM C07K016-04

ICS C07K014-47; C07K001-36; A23C009-14

NCL 530366000

CC 9-9 (Biochemical Methods)

Section cross-reference(s): 15, 17

FAN.CNT 2

	PATENT NO.	KIND	DATE	APPLICATION NO.	DATE
PI	US 5756680	A	19980526	US 1996-678364	19960716 <--
	US 6096870	A	20000801	US 1998-76169	19980504 <--
PRAI	US 1994-177574	B1	19940105 <--		
	US 1996-678364	A2	19960716 <--		

AB A method is disclosed for the sequential sepn. of whey proteins using radial-flow chromatog. Different buffer systems adjusted to suitable pH and ionic strength are utilized in the sepn. process. The method separates at least five different proteins, e.g lactoferrin, Ig, lactoglobulin, **lactalbumin** and bovine serum albumin, from whey. Infant feeding formulas, and other food formulations are also disclosed incorporating therein in different proportions various proteins sepd. from the whey.

ST whey protein radial flow chromatog column; infant formula lactoferrin Ig lactoglobulin **lactalbumin**

IT Immunoglobulins

RL: FFD (Food or feed use); PUR (Purification or recovery); BIOL

(Biological study); PREP (Preparation); USES (Uses)

(G; sequential sepn. of whey proteins and formulations thereof)

IT Albumins, biological studies

RL: FFD (Food or feed use); PUR (Purification or recovery); BIOL (Biological study); PREP (Preparation); USES (Uses)
(bovine serum; sequential sepn. of whey proteins and formulations thereof)

IT Milk
(cow or human; sequential sepn. of whey proteins and formulations thereof)

IT Milk substitutes
(human; sequential sepn. of whey proteins and formulations thereof)

IT Caseins, biological studies
RL: FFD (Food or feed use); BIOL (Biological study); USES (Uses)
(hydrolyzates; sequential sepn. of whey proteins and formulations thereof)

IT Dairy products
(nonfat milk solid; sequential sepn. of whey proteins and formulations thereof)

IT Buffers
Cation exchangers
Liquid chromatography
(sequential sepn. of whey proteins and formulations thereof)

IT Carbohydrates, biological studies
Fats and Glyceridic oils, biological studies
Minerals, biological studies
Vitamins
RL: FFD (Food or feed use); BIOL (Biological study); USES (Uses)
(sequential sepn. of whey proteins and formulations thereof)

IT Immunoglobulins
Lactalbumins
Lactoferrins
Lactoglobulins
RL: FFD (Food or feed use); PUR (Purification or recovery); BIOL (Biological study); PREP (Preparation); USES (Uses)
(sequential sepn. of whey proteins and formulations thereof)

IT Proteins, specific or class
RL: FFD (Food or feed use); PUR (Purification or recovery); BIOL (Biological study); PREP (Preparation); USES (Uses)
(whey; sequential sepn. of whey proteins and formulations thereof)

IT **Lactalbumins**
RL: FFD (Food or feed use); PUR (Purification or recovery); BIOL (Biological study); PREP (Preparation); USES (Uses)
(.alpha.-; sequential sepn. of whey proteins and formulations thereof)

IT **Lactalbumins**
RL: REM (Removal or disposal); PROC (Process)
(.beta.-; sequential sepn. of whey proteins and formulations thereof)

RE.CNT 12 THERE ARE 12 CITED REFERENCES AVAILABLE FOR THIS RECORD

RE

(1) Burling; US 5149647 1992 HCPLUS
(2) Chaveron; US 4803089 1989 HCPLUS
(3) Derahm; US 4879131 1989 HCPLUS
(4) Girardet; Milchwissencharft 1989, V44(11), P692 HCPLUS
(5) Host; Allergy 1992, V47(3), P218 MEDLINE
(6) Kakade; US 4614653 1986 HCPLUS
(7) Kulczjcki; US 5223281 1993
(8) Kuwata; US 4834994 1989 HCPLUS
(9) Manji; J Dairy Sci 1985, V68, P3176 HCPLUS
(10) Saxena; US 4865729 1989 HCPLUS
(11) Thibault; US 5077067 1991 HCPLUS
(12) Uchida; US 5179197 1993

TI Bovine whey fractionation based on cation-exchange chromatography
AU Hahn, R.; Schulz, P. M.; Schaupp, C.; Jungbauer, A.
CS Forestry and Biotechnology, Institute of Applied Microbiology, University
of Agriculture, Muthgasse 18, Vienna, A-1190, Austria
SO Journal of Chromatography, A (1998), 795(2), 277-287
CODEN: JCRAEY; ISSN: 0021-9673
PB Elsevier Science B.V.
DT Journal
LA English
CC 9-3 (Biochemical Methods)
Section cross-reference(s): 17
AB Bovine whey proteins have potential applications in veterinary medicine,
food industry and as supplements for cell culture media. A fractionation
scheme for the economically interesting proteins, such as IgG, lactoferrin
and lactoperoxidase, based on cation exchangers was the goal of our
investigations. A chromatog. process was developed where *.alpha*-
-lactalbumin passes through the column and sepn. of the desired
proteins is achieved. Four different cation-exchange media (S-HyperD-F,
S-Sepharose FF, Fractogel EMD SO3- 650 (S) and Macro-Prep High S Support)
were compared in regard to their dynamic binding capacity for IgG and
their different elution behaviors when sequential step gradients with NaCl
buffers were applied. Peak fractions were analyzed by size-exclusion
chromatog. and sodium dodecyl sulfate-polyacrylamide gel electrophoresis.
Lactoperoxidase activity was monitored by the oxidn. of
o-phenylenediamine. In order to explain the different resoln. behaviors,
isocratic runs with pure stds. of whey proteins were performed. The k'
values were calcd. and plotted against salt concn. Fractogel EMD had the
highest binding capacity for IgG, 3.7 mg/mL gel at a linear flow-rate of
100 cm/h, but the resoln. was low compared to that with the other three
media. S-Hyper D and S-Sepharose FF showed lower capacities, 3.3 and 3.2
mg/mL gel, resp., but exhibited better protein resoln. These effects
could be partially explained by the k' vs. salt concn. plots. The binding
capacity of Macro-Prep S was considerably lower compared to that of the
other resins investigated because its selectivity for whey proteins was
completely different. S-Sepharose FF and S-Hyper D combine relatively
high dynamic capacity for IgG and good resoln. Compared to studies with
std. proteins, such as 100 mg/mL bovine serum albumin for S-Hyper D, their
binding capacities were very low. Even after removal of low-mol.-mass
compds., the capacity could not be improved significantly. The running
conditions (low pH) were responsible for the low protein binding capacity,
since low-mol.-mass compds. in the feed do not compete with the adsorption
of whey protein. The dynamic capacity did not decrease to a large extent
within the range of flow-rates (100-600 cm/h) investigated. The dynamic
capacity of HyperD and Fractogel was at least five times higher when pure
bovine IgG was used for detn. In conclusion, S-Sepharose FF, S-Hyper D-F
and Fractogel EMD SO3- 650 (S) are considered as successful candidates for
the large-scale purifn. of bovine whey proteins.
ST whey protein purifn cation exchange chromatog
IT Immunoglobulins
RL: PUR (Purification or recovery); PREP (Preparation)
(G; bovine whey fractionation based on cation-exchange chromatog.)
IT Cation exchange chromatography
Whey
(bovine whey fractionation based on cation-exchange chromatog.)
IT Lactoferrins
Proteins, general, preparation
RL: PUR (Purification or recovery); PREP (Preparation)
(bovine whey fractionation based on cation-exchange chromatog.)
IT Proteins, specific or class
RL: PEP (Physical, engineering or chemical process); PROC (Process)
(whey; bovine whey fractionation based on cation-exchange chromatog.)
IT Lactalbumins
RL: PUR (Purification or recovery); PREP (Preparation)

(.alpha.-; bovine whey fractionation based on cation-exchange chromatog.)

IT Lactoglobulins

RL: PUR (Purification or recovery); PREP (Preparation)

(.beta.-; bovine whey fractionation based on cation-exchange chromatog.)

IT 129186-25-0, Fractogel EMD 133976-91-7, Sepharose FF 188039-62-5, Macro-Prep High S 189303-29-5, HyperD

RL: PEP (Physical, engineering or chemical process); PROC (Process) (bovine whey fractionation based on cation-exchange chromatog.)

IT 9003-99-0P, Lactoperoxidase

RL: PUR (Purification or recovery); PREP (Preparation)

(bovine whey fractionation based on cation-exchange chromatog.)

L86 ANSWER 11 OF 21 HCPLUS COPYRIGHT 2003 ACS

AN 1997:43849 HCPLUS

DN 126:117185

TI Whey proteins extraction by fluidized ion exchange

chromatography: simplified modeling and economical optimization

AU Carrere, H.; Bascoul, A.; Floquet, P.; Wilhelm, A. M.; Delmas, H.

CS Laboratoire de Genie Chimique, Unite de Recherche CNRS 5503, ENSIGC, 18 chemin de la Loge, Toulouse, 31078, Fr.

SO Chemical Engineering Journal (Lausanne) (1996), 64(3), 307-317
CODEN: CMEJAJ; ISSN: 0300-9467

PB Elsevier

DT Journal

LA English

CC 17-2 (Food and Feed Chemistry)

AB A study was made of sweet whey protein (.alpha.-lactalbumin and .beta.-lactoglobulin) recovery by a fluidized ion exchange chromatog. process. Simplified models are proposed for both main steps of this cyclic process: a model with intraparticle diffusion for the adsorption of proteins (fixation step) and a lumped kinetic model for their desorption (elution step). The validity of these models and their phys. background are discussed. They are then used for an economical optimization algorithm in order to det. operating conditions (duration of fixation and elution steps, elution effluent recycling and liq.-phase velocity). Recycling the elution effluents leads to a slight improvement in the process but it was found to be less advantageous than an optimization of the liq.-phase velocity.

ST whey protein extn ion exchange chromatog

IT Simulation and Modeling, physicochemical (of whey protein extn. by fluidized ion exchange chromatog.)

IT Ion exchange chromatography

(preparative fluidized; modeling of whey protein extn. by fluidized ion exchange chromatog.)

IT Proteins, specific or class

RL: PUR (Purification or recovery); PREP (Preparation)

(whey; modeling of whey protein extn. by fluidized ion exchange chromatog.)

IT Lactalbumins

RL: PUR (Purification or recovery); PREP (Preparation)

(.alpha.-; modeling of whey protein extn. by fluidized ion exchange chromatog.)

IT Lactoglobulins

RL: PUR (Purification or recovery); PREP (Preparation)

(.beta.-; modeling of whey protein extn. by fluidized ion exchange chromatog.)

L86 ANSWER 12 OF 21 HCPLUS COPYRIGHT 2003 ACS

AN 1996:574639 HCPLUS

DN 125:219927

TI Fractionation of proteins from whey with different pilot scale processes
AU Outinen, M.; Tossavainen, O.; Tupasela, T.; Koskela, P.; Koskinen, H.;
Rantamaki, P.; Syvaoja, E.-L.; Antila, P.; Kankare, V.
CS R&D Cent., Valio Ltd., Helsinki, FIN-00101, Finland
SO Food Science & Technology (London) (1996), 29(5 & 6), 411-417
CODEN: LBWTAP; ISSN: 0023-6438
PB Academic
DT Journal
LA English
CC 17-2 (Food and Feed Chemistry)
Section cross-reference(s): 6
AB Pilot scale prodn. of .alpha.-lactalbumin (.alpha.-La) and .beta.-lactoglobulin (.beta.-Lg) from sweet and acid casein wheys using two heat pptn. and two chromatog. methods was studied. Using the heat pptn. methods, the sol. .beta.-Lg was recovered easily by ultrafiltration, but the recovery of the low d. .alpha.-La ppt. was difficult. In addn., with acid casein whey, significant denaturation of .alpha.-La occurred. .beta.-Lg was selectively removed from acid casein whey with strongly basic silica and polystyrene anion exchange resin columns by elution with 0.1 mol/L HCl or 0.33 mol/L NaCl soln. .beta.-Lg eluted with HCl was highly denatured.
ST protein fractionation whey pilot scale process; lactalbumin fractionation whey pilot scale process; lactoglobulin fractionation whey pilot scale process
IT Whey
(fractionation of proteins from whey with different pilot scale processes)
IT Chromatography, column and liquid
(ion-exchange, fractionation of proteins from whey with different pilot scale processes)
IT Filtration
(ultra-, fractionation of proteins from whey with different pilot scale processes)
IT Lactalbumins
RL: PUR (Purification or recovery); PREP (Preparation)
(.alpha.-, fractionation of proteins from whey with different pilot scale processes)
IT Lactoglobulins
RL: PUR (Purification or recovery); PREP (Preparation)
(.beta.-, fractionation of proteins from whey with different pilot scale processes)
IT 7647-01-0, Hydrochloric acid, biological studies 7647-14-5
, Sodium chloride, biological studies
RL: BUU (Biological use, unclassified); PEP (Physical, engineering or chemical process); BIOL (Biological study); PROC (Process); USES (Uses)
(fractionation of proteins from whey with different pilot scale processes)
IT 7647-01-0, Hydrochloric acid, biological studies 7647-14-5
, Sodium chloride, biological studies
RL: BUU (Biological use, unclassified); PEP (Physical, engineering or chemical process); BIOL (Biological study); PROC (Process); USES (Uses)
(fractionation of proteins from whey with different pilot scale processes)
RN 7647-01-0 HCPLUS
CN Hydrochloric acid (6CI, 7CI, 8CI, 9CI) (CA INDEX NAME)

HCl

RN 7647-14-5 HCPLUS
CN Sodium chloride (NaCl) (9CI) (CA INDEX NAME)

Cl-Na

L86 ANSWER 13 OF 21 HCPLUS COPYRIGHT 2003 ACS
 AN 1996:340682 HCPLUS
 DN 125:1356
 TI Antibacterial composition containing multimeric .alpha.-lactalbumin
 IN Sabharwal, Hemant; Svanborg, Catharina
 PA Swed.
 SO PCT Int. Appl., 34 pp.
 CODEN: PIXXD2
 DT Patent
 LA English
 IC ICM A61K038-38
 ICS A61K035-20
 CC 1-5 (Pharmacology)
 FAN.CNT 1

	PATENT NO.	KIND	DATE	APPLICATION NO.	DATE
PI	WO 9604929	A1	19960222	WO 1994-SE742	19940816
	W: AU, BR, CA, CZ, FI, HU, JP, KR, NO, NZ, PL, RU, SK, US RW: AT, BE, CH, DE, DK, ES, FR, GB, GR, IE, IT, LU, MC, NL, PT, SE, BF, BJ, CF, CG, CI, CM, GA, GN, ML, MR, NE, SN, TD, TG				
	CA 2197659	AA	19960222	CA 1994-2197659	19940816
	AU 9477922	A1	19960307	AU 1994-77922	19940816
	EP 776214	A1	19970604	EP 1994-928519	19940816
	EP 776214	B1	19990728	R: AT, BE, CH, DE, DK, ES, FR, GB, GR, IE, IT, LI, LU, NL, PT, SE	
	JP 10504547	T2	19980506	JP 1994-507224	19940816
	AT 182470	E	19990815	AT 1994-928519	19940816
	ES 2136206	T3	19991116	ES 1994-928519	19940816
PRAI	EP 1994-928519		19940816		
	WO 1994-SE742		19940816		

Concluded

AB A multimeric .alpha.-lactalbumin (I) is sepd from milk and used in the therapeutic or prophylactic treatment and/or for diagnostic use for infections, preferably of the respiratory tract, caused by bacteria, in particular *S. pneumoniae* and/or *H. influenzae*.

Antiadhesive and bactericidal .alpha.-lactalbumin was purified from human breast milk by fractionation of casein by ion exchange chromatog. and fractionation of the pool eluting after 1M NaCl by gel chromatog. Antibiotic-resistant *Streptococcus pneumoniae* was incubated with 10 mg/mL I for 0.5 h then it was inoculated onto growth plate. There was no viable counts as compared with 1×10^6 for the untreated controls.

ST antibacterial compn alpha lactalbumin breast milk

IT Bactericides, Disinfectants, and Antiseptics

Haemophilus influenzae

Streptococcus pneumoniae

(antibacterial compn. contg. multimeric .alpha.-lactalbumin)

IT Milk

(breast; antibacterial compn. contg. multimeric .alpha.-lactalbumin)

IT Lactalbumins

RL: BAC (Biological activity or effector, except adverse); BOC (Biological occurrence); BSU (Biological study, unclassified); THU (Therapeutic use); BIOL (Biological study); OCCU (Occurrence); USES (Uses)

(.alpha.-, antibacterial compn. contg. multimeric alpha-lactalbumin)

L86 ANSWER 14 OF 21 HCPLUS COPYRIGHT 2003 ACS
 AN 1996:322517 HCPLUS
 DN 125:84961
 TI Recovery of whey proteins in a fluidized bed: effect of solid-phase mixing
 AU Mourad, M.; Bascoul, A.; Delmas, H.; Wilhelm, A. M.; Gros, B.
 CS Lab. Genie Chimique, ENSIGC, Toulouse, 31078, Fr.
 SO Recents Progres en Genie des Procedes (1995), 9(42), Genie des
 Procedes Complexes, 483-488
 CODEN: RPGPEX; ISSN: 1166-7478
 PB Tec & Doc - Lavoisier
 DT Journal
 LA French
 CC 17-2 (Food and Feed Chemistry)
 AB A model was developed for recovery of .alpha.-lactalbumin and .beta.-lactoglobulin from whey by ion-exchange chromatog. in a fluidized bed. The model is based on two compartments; in the first, solid and liq. phases flow cocurrently; there is countercurrent flow in the second compartment. Simulations of the effect of bed height indicated that above a value of 7 cm the fixation of proteins occurs in three steps and solid-phase mixing has a controlling influence on adsorption.
 ST whey protein recovery fluidized bed model; ion exchange chromatog whey protein
 IT Fluidized beds and systems
 Simulation and Modeling, biological
 Whey
 (recovery of whey proteins in fluidized beds in relation to solid-phase mixing)
 IT Lactalbumins
 RL: PUR (Purification or recovery); PREP (Preparation)
 (.alpha.-, recovery of whey proteins in fluidized beds in relation to solid-phase mixing)
 IT Lactoglobulins
 RL: PUR (Purification or recovery); PREP (Preparation)
 (.beta.-, recovery of whey proteins in fluidized beds in relation to solid-phase mixing)

L86 ANSWER 15 OF 21 HCPLUS COPYRIGHT 2003 ACS
 AN 1996:199189 HCPLUS
 DN 124:287502
 TI Preparative ion exchange chromatography of protein from dairy whey (lactose)
 AU Gerberding, Steven Jay
 CS Univ. of Tennessee, Knoxville, TN, USA
 SO (1996) 227 pp. Avail.: Univ. Microfilms Int., Order No. DA9609291
 From: Diss. Abstr. Int., B 1996, 56(11), 6257
 DT Dissertation
 LA English
 CC 17-8 (Food and Feed Chemistry)
 AB Unavailable
 ST whey protein chromatog
 IT Whey
 (preparative ion exchange chromatog. of protein from dairy whey)
 IT Albumins, preparation
 Proteins, preparation
 RL: PUR (Purification or recovery); PREP (Preparation)
 (preparative ion exchange chromatog. of protein from dairy whey)
 IT Immunoglobulins
 RL: PUR (Purification or recovery); PREP (Preparation)
 (G, preparative ion exchange chromatog.

of protein from dairy whey)
IT Chromatography, column and liquid
(ion-exchange, preparative ion
exchange chromatog. of protein from dairy whey)
IT Lactalbumins
RL: PUR (Purification or recovery); PREP (Preparation)
(.alpha.-, preparative ion exchange
chromatog. of protein from dairy whey)
IT Lactoglobulins
RL: PUR (Purification or recovery); PREP (Preparation)
(.beta.-, preparative ion exchange
chromatog. of protein from dairy whey)

L86 ANSWER 16 OF 21 HCAPLUS COPYRIGHT 2003 ACS
AN 1995:892334 HCAPLUS
DN 123:312543
TI Quantitative chromatographic separation of milk proteins
AU Franzen, Maike; Pabst, K.; Schulte-Coerne, H.; Gravert, H. O.
CS Bundesanstalt Milchforschung, Kiel, 24103, Germany
SO Milchwissenschaft (1995), 50(9), 483-8
CODEN: MILCAD; ISSN: 0026-3788
PB VV-GmbH Volkswirtschaftlicher Verlag
DT Journal
LA German
CC 17-8 (Food and Feed Chemistry)
Section cross-reference(s): 13
AB Samples of milk were taken from 778 black pied cows and 368 cows of the
Angler breed during the period from Jan. to May, 1990, and analyzed
concerning their protein fraction contents by means of HPLC. The protein
fraction contents varied considerably between cows. They depended on the
herd level, the stage of lactation and the cows' age as well. The high
performance ion-exchange chromatog. of the
major bovine milk proteins is an alternative method to electrophoresis
with densitometry for the qual. and quant. anal. of milk proteins. The
successful sepn. and identification of whey proteins and caseins showed us
that with this method complex biol. systems could be analyzed.
ST milk protein purifn sepn HPLC
IT Milk
Senescence
Whey
(quant. chromatog. sepn. of and factors affecting milk proteins)
IT Albumins, biological studies
Caseins, biological studies
Immunoglobulins
Proteins, biological studies
RL: BOC (Biological occurrence); BSU (Biological study, unclassified); PUR
(Purification or recovery); BIOL (Biological study); OCCU (Occurrence);
PREP (Preparation)
(quant. chromatog. sepn. of and factors affecting milk proteins)
IT Lactation
(stage; quant. chromatog. sepn. of and factors affecting milk proteins)
IT Chromatography, column and liquid
(high-performance, quant. chromatog. sepn. of and factors affecting
milk proteins)
IT Caseins, biological studies
RL: BOC (Biological occurrence); BSU (Biological study, unclassified); PUR
(Purification or recovery); BIOL (Biological study); OCCU (Occurrence);
PREP (Preparation)
(.kappa.-, quant. chromatog. sepn. of and factors affecting milk
proteins)
IT Lactalbumins
RL: BOC (Biological occurrence); BSU (Biological study, unclassified); PUR
(Purification or recovery); BIOL (Biological study); OCCU (Occurrence);

PREP (Preparation)

(.alpha.-, quant. chromatog. sepn. of and factors affecting
milk proteins)

IT Caseins, biological studies

RL: BOC (Biological occurrence); BSU (Biological study, unclassified); PUR (Purification or recovery); BIOL (Biological study); OCCU (Occurrence);
PREP (Preparation)

(.alpha.s-, quant. chromatog. sepn. of and factors affecting
milk proteins)

IT Caseins, biological studies

Lactoglobulins

RL: BOC (Biological occurrence); BSU (Biological study, unclassified); PUR (Purification or recovery); BIOL (Biological study); OCCU (Occurrence);
PREP (Preparation)

(.beta.-, quant. chromatog. sepn. of and factors affecting milk
proteins)

IT Caseins, biological studies

RL: BOC (Biological occurrence); BSU (Biological study, unclassified); PUR (Purification or recovery); BIOL (Biological study); OCCU (Occurrence);
PREP (Preparation)

(.gamma.-, quant. chromatog. sepn. of and factors affecting milk
proteins)

L86 ANSWER 17 OF 21 HCPLUS COPYRIGHT 2003 ACS

AN 1993:100823 HCPLUS

DN 118:100823

TI Manufacture of composition with high **alpha-lactalbumin**
content from whey

IN Shimatani, Masaharu; Uchida, Yukio; Matsuno, Ichirou; Sugawara, Makihiro;
Nakano, Taku

PA Snow Brand Milk Products Co., Ltd., Japan

SO Fr. Demande, 13 pp.

CODEN: FRXXBL

DT Patent

LA French

IC ICM A23C021-00

ICS A23C009-146

ICA A61K037-02

CC 17-8 (Food and Feed Chemistry)

FAN.CNT 1

	PATENT NO.	KIND	DATE	APPLICATION NO.	DATE
PI	FR 2671697	A1	19920724	FR 1992-545	19920120 <--
	FR 2671697	B1	20010727		
	JP 04330252	A2	19921118	JP 1991-19114	19910121 <--
	JP 2961625	B2	19991012		
	AU 650719	B2	19940630	AU 1992-11301	19920227 <--
	AU 9211301	A1	19930909		
	US 5434250	A	19950718	US 1994-231984	19940421 <--
PRAI	JP 1991-19114	A	19910121 <--		
	US 1992-820369	B1	19920114 <--		

AB A method for prep. an **alpha-lactalbumin** conc.
comprises (a) adjusting the pH of whey obtained from cheese or casein
manuf. to .gtoreq.5; (b) contacting the whey with an ion exchanger; (c)
adjusting the pH of soln. obtained from the ion exchanger treatment to
.ltoreq.4; and (d) concg. or desalting the soln. The soln. from step b
may be concd. and the lactose removed by crystn. In step d, the soln. is
subjected to ultrafiltration. Using this procedure, 100 kg of whey was
processed to produce 8 kg soln. contg. 4.2 g **alpha-lactalbumin**/100 g soln.
This soln. was concd. and dried to obtain 0.90 kg powder.

ST **lactalbumin alpha whey ion exchanger**

IT **Anion exchangers**

Cation exchangers
 (in .alpha.-lactalbumin manuf. from whey, pH in relation to)

IT Whey
 (.alpha.-lactalbumin conc. manuf. from, with ion exchangers, pH in relation to)

IT Filtration
 (ultra-, in .alpha.-lactalbumin manuf. from whey, pH in relation to)

IT Lactalbumins
 RL: PREP (Preparation)
 (.alpha.-, prepn. of, from whey, with ion exchangers, pH in relation to)

IT 144746-90-7, Indion S 3 145018-76-4, Sepharosil MAQ
 RL: BIOL (Biological study)
 (in .alpha.-lactalbumin conc. prepn. from whey, pH in relation to)

IT 63-42-3, Lactose
 RL: REM (Removal or disposal); PROC (Process)
 (removal of, from treated whey, for prepn. of .alpha.-lactalbumin conc.)

L86 ANSWER 18 OF 21 HCPLUS COPYRIGHT 2003 ACS

AN 1990:196885 HCPLUS

DN 112:196885

TI Method for fractionating proteins of human milk leading to the production particularly of lactoferrin and (alpha)-lactalbumin, and products obtained

IN Maynard, Francoise; Pierre, Alice; Maubois, Jean Louis

PA Institut National de la Recherche Agronomique, Fr.

SO PCT Int. Appl., 32 pp.

CODEN: PIXXD2

DT Patent

LA French

IC ICM A23J001-20

ICS A23C009-142; A61K035-20; A61K037-02

CC 17-6 (Food and Feed Chemistry)

FAN.CNT 1

	PATENT NO.	KIND	DATE	APPLICATION NO.	DATE
PI	WO 8911226	. A1	19891130	WO 1989-FR255	19890526 <--
	W: AU, DK, JP, NO, US				
	RW: AT, BE, CH, DE, FR, GB, IT, LU, NL, SE				
	FR 2631785	A1	19891201	FR 1988-7122	19880527 <--
	AU 8937493	A1	19891212	AU 1989-37493	19890526 <--
PRAI	FR 1988-7122		19880527 <--		
	WO 1989-FR255		19890526 <--		
AB	Human milk proteins are fractionated at <48.degree. to produce lactoferrin, .alpha.-lactalbumin, and other products by microfiltration with a membrane of pore size .apprx.0.2 .mu.m, ultrafiltration with an 80,000-300,000 (preferably .apprx.100,000) daltons threshold mol. wt., and then further ultrafiltration (threshold mol. wt. preferably 10,000). With addnl. diafiltration, plus ion exchange chromatog., the lactalbumin of the retentate after the 1st ultrafiltration is purified (with removal of minor amts. of serum albumin by this process). Diafiltration of the retentate after the 2nd ultrafiltration step purifies the .alpha.-lactalbumin. The products may be used as therapeutic or dietetic dietary constituents for humans or animals.				

ST milk protein fractionation lactalbumin lactoferrin

IT Feed

(dietetic and therapeutic, .alpha.-lactalbumin and lactoferrin from human milk purifn. for)

IT Proteins, biological studies
 RL: BIOL (Biological study)
 (of human milk, fractionation of)
 IT Albumins, biological studies
 Lactoferrins
 RL: PUR (Purification or recovery); PREP (Preparation)
 (purifn. of, from human milk proteins by microfiltration and
 ultrafiltration)
 IT Food
 (dietetic, lactoferrin and .alpha.-lactalbumin from
 human milk purifn. for)
 IT Milk
 (human, proteins of, fractionation of)
 IT Filtration
 (micro-, of milk proteins of humans, lactoferrin and .alpha.-
 lactalbumin fractionation and purifn. by)
 IT Food
 (therapeutic, lactoferrin and .alpha.-lactalbumin
 from human milk purifn. for)
 IT Filtration
 (ultra-, of milk proteins of humans, lactoferrin and .alpha.-
 lactalbumin fractionation and purifn. by)
 IT Lactalbumins
 RL: PUR (Purification or recovery); PREP (Preparation)
 (.alpha.-, purifn. of, from human milk proteins by
 microfiltration and ultrafiltration)

L86 ANSWER 19 OF 21 HCAPLUS COPYRIGHT 2003 ACS
 AN 1982:404926 HCAPLUS
 DN 97:4926
 TI Animal or vegetable protein preparation, specifically lactoproteins and
 their products
 IN Arnaud, Michel; Chambon, Michel; Edon, Andre; Guillet, Nicole; Malige,
 Bernard
 PA Fromageries Bel S. A., Fr.
 SO Fr. Demande, 12 pp.
 CODEN: FRXXBL
 DT Patent
 LA French
 IC A23J001-20; A23J003-00
 ICA A23C009-00; A23C019-00; A23K001-08
 CC 17-8 (Food and Feed Chemistry)
 FAN.CNT 2

	PATENT NO.	KIND	DATE	APPLICATION NO.	DATE
PI	FR 2452881	A1	19801031	FR 1979-8555	19790404 <--
	FR 2452881	B1	19831125		
	FR 2487642	A2	19820205	FR 1980-16970	19800731 <--
	FR 2487642	B2	19851018		

PRAI FR 1979-8555 19790404 <--

AB Proteins with properties of interest in the food industry are prep'd. by
 ion-exchange and exclusion chromatog. from raw
 materials (esp. whey, milk, and buttermilk) subjected to physicochem.
 pretreatments. Among the products that can be obtained are .alpha
 .-lactalbumin for use in human milk substitutes, fractions rich
 in SH groups for use in bakery products, and milk without serum proteins
 for use in cheese manuf. Thus, sweet whey was concd. and brought to pH
 6.5 with NH4OH. The soln. was cooled to .apprx.5.degree., then percolated
 through 3 columns arranged in the series: anionic, cationic, then anionic
 column. From the 1st column .beta.-lactoglobulin, from the 2nd globulins,
 and from the 3rd .alpha.-lactalbumins were isolated.
 ST protein sepn milk chromatog; ion exchange protein milk; whey protein sepn
 chromatog

IT Milk
 Whey
 (proteins of, chromatog. sepn. of, for food manuf.)
 IT Lactalbumins
 Lactoglobulins
 RL: PUR (Purification or recovery); PREP (Preparation)
 (purifn. of, for food manuf.)
 IT Lactalbumins
 RL: PUR (Purification or recovery); PREP (Preparation)
 (.alpha.-, purifn. of, for food manuf.)

L86 ANSWER 20 OF 21 HCPLUS COPYRIGHT 2003 ACS
 AN 1980:127014 HCPLUS
 DN 92:127014
 TI Purification of whey proteins for quantitative electrophoresis
 AU Reimerdes, E. H.; Mehren, H. A.; Matthiesen, Inge
 CS Bundesanst. Milchforsch., Inst. Chem. Phys., Kiel, Fed. Rep. Ger.
 SO Kieler Milchwirtschaftliche Forschungsberichte (1979), 31(3),
 223-37
 CODEN: KMWFAF; ISSN: 0023-1347
 DT Journal
 LA German
 CC 17-1 (Foods)
 Section cross-reference(s): 9
 AB .beta.-Lactoglobulins A and B, .alpha.-lactalbumin,
 and serum albumin were isolated from whey obtained from skim milk by pptg.
 casein with HCl at pH 4.6, dialyzing 12-15 h, and freeze drying the whey
 protein. The albumins were sepd. by anion exchange on a DEAE-cellulose DE
 52 column with pH 7.2 Tris-HCl buffers in a Tris gradient of 0.01-0.25 N.
 Protein-contg. eluate fractions were dialyzed and freeze dried for addn.
 fractionation on a Sepahdex G-100 with a pH 6.1 buffer contg. 0.1N
 Tris-HCl and 1M NaCl. Lactoglobulins were sepd. by salt pptn. followed by
 ion exchange or gel chromatog. Thus, 264 g
 $(\text{NH}_4)_2\text{SO}_4$ was added slowly to 1 L fresh raw milk at 20.degree. with
 stirring, fat and casein were removed by centrifuging at 1200 g for 30
 min, and the whey was filtered and preserved with PhMe. The pH was
 adjusted to 3.5 with 1N HCl to obtain an .alpha.-
 lactalbumin-rich fraction by centrifugation (14,000 g for 40 min).
 The supernatant was filtered, adjusted to pH 6 with 1N NH4OH, 264 g/L
 $(\text{NH}_4)_2\text{SO}_4$ added, and a lactoglobulin-rich fraction was obtained by
 centrifuging. This fraction was desalted by chromatog. on a column of
 Sephadex G-15, eluting with H2O or on Ultrogel AcA 44 mol. sieve, eluting
 with 0.2% NaCl for fractionation. The protein-contg. eluate fractions
 were dialyzed and freeze dried. Polyacrylamide gel electrophoresis was
 used to control the fractionations.
 ST whey protein fractionation; lactalbumin purifn; lactoglobulin
 purifn; serum albumin purifn
 IT Whey
 (proteins of, fractionation and purifn. of)
 IT Albumins, blood serum
 RL: PUR (Purification or recovery); PREP (Preparation)
 (purifn. of, from whey)
 IT Lactalbumins
 RL: PUR (Purification or recovery); PREP (Preparation)
 (.alpha.-, purifn. of, from whey)
 IT Lactoglobulins
 RL: BIOL (Biological study)
 (.beta.-, A and B, purifn. of, from whey)

L86 ANSWER 21 OF 21 HCPLUS COPYRIGHT 2003 ACS
 AN 1973:109368 HCPLUS
 DN 78:109368
 TI Simple procedures for the separation and identification of bovine milk

whey proteins
AU Cervone, Felice; Diaz Brito, Joaquin; Di Prisco, Guido; Garofano, Felice;
Gutierrez Norona, Lilliam; Traniello, Serena; Zito, Romano
CS Sch. Pharm. Biochem., Univ. La Habana, Havana, Cuba
SO Biochimica et Biophysica Acta (1973), 295(2), 555-63
CODEN: BBACAO; ISSN: 0006-3002
DT Journal
LA English
CC 17-1 (Foods)
Section cross-reference(s): 9
AB A simple procedure, ion-exchange column chromatog. on DEAE-cellulose, is described, which allows complete sepn. of the major components of bovine milk whey. Electrophoretically pure .alpha.-lactalbumin B, .beta.-lactoglobulin A, and .beta.-lactoglobulin B are eluted with a linear concn. gradient at const. pH; serum albumin is eluted in another peak, but is assocd. with another whey protein. The fractionation can be achieved also on a preparative scale, starting either from (NH4)2SO4 whey or neutralized acid whey; prior concn. is unnecessary. Rapid electrophoretic techniques, which permit identification of whey proteins, as well as simultaneous anal. of whey from a large no. of individual animals, in 40-90 min, are also described.
ST milk whey protein chromatog; electrophoresis whey protein
IT Milk analysis
 (protein sepn. in)
IT Whey
 (proteins of, prep. of)
IT Proteins
 RL: PROC (Process)
 (sepn. of, of whey)
IT Lactalbumins
 RL: SPN (Synthetic preparation); PREP (Preparation)
 (.alpha.-, B, prep. of)
IT Lactoglobulins
 RL: SPN (Synthetic preparation); PREP (Preparation)
 (.beta.-, A and B, prep. of)

=> fil wpix
FILE 'WPIX' ENTERED AT 12:35:49 ON 27 MAR 2003
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FILE LAST UPDATED: 24 MAR 2003 <20030324/UP>
MOST RECENT DERWENT UPDATE: 200320 <200320/DW>
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GUIDES, PLEASE VISIT:
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=> d all abeq tech abex tot

L114 ANSWER 1 OF 17 WPIX (C) 2003 THOMSON DERWENT
AN 2000-578416 [54] WPIX
DNC C2000-172153
TI Novel methods for separation of whey proteins, useful as nutritional supplements, comprising passing whey through cationic and anionic columns.
DC A96 B04 D13
IN AHMED, S H; MIRANDA, Q R; MOZAFFAR, Z; SAXENA, V
PA (SEPR-N) SEPRAGEN CORP
CYC 1
PI US 6096870 A 20000801 (200054)* 47p C07K016-04
ADT US 6096870 A Cont of US 1994-177574 19940105, CIP of US 1996-678364 19960716, US 1998-76169 19980504
FDT US 6096870 A CIP of US 5756680
PRAI US 1998-76169 19980504; US 1994-177574 19940105; US 1996-678364 19960716
IC ICM C07K016-04
ICS A23C009-12; C07K014-47
AB US 6096870 A UPAB: 20001027
NOVELTY - Sequential separation of whey proteins (I), comprising passing a whey sample comprising immunoglobulins, beta-lactoglobulin, **alpha**-lactalbumin, lactoperoxidase, serum albumin and/or lactoferrin through a cationic exchange resin, collecting the flow-through, and (sequentially) eluting the immunoglobulins, beta-lactoglobulin, **alpha**-lactalbumin, serum albumin, lactoferrin and lactoperoxidase from the resin.

DETAILED DESCRIPTION - Sequential separation of whey proteins (I), comprising passing a whey sample comprising immunoglobulins, beta-lactoglobulin, **alpha**-lactalbumin, lactoperoxidase, serum albumin and/or lactoferrin through a cationic exchange resin under adsorbent conditions, collecting the flow-through (comprising lactose, minerals, lactic acid, and non-nitrogenous components), and (sequentially) eluting the immunoglobulins, beta-lactoglobulin, **alpha**-lactalbumin, serum albumin, lactoferrin and lactoperoxidase from the resin.

INDEPENDENT CLAIMS are also included for the following:

(1) a 2-column method for the separation of whey proteins comprising passing a whey sample through an anionic exchange resin, collecting the flow-through (containing immunoglobulins, **alpha**-lactalbumin, lactoperoxidase, serum albumin and/or lactoferrin) and eluting beta-lactoglobulin from the resin, passing the flow-through through an ultrafiltration membrane, passing the ultrafiltrate through a cation exchange resin and sequentially eluting immunoglobulins, **alpha**-lactalbumin, serum albumin and lactoferrin from the resin;

(2) processing whey comprising passing a whey sample through a cation exchange resin and collecting the deproteinized whey flow-through;

(3) production of a clear whey protein isolate comprising passing a whey sample through a cation exchange resin, and sequentially eluting the whey proteins adsorbed onto the resin, and serum albumin and fat from the resin;

(4) production of an **alpha**-lactalbumin-enriched whey protein isolate comprising passing whey through an anion exchange resin under conditions that promote the binding of beta-lactalbumin but not **alpha**-lactalbumin; and

(5) cleaning a resin contained within a chromatography column comprising washing the resin with sodium hypochlorite and sequentially exposing the washed resin to sodium hydroxide, hydrochloric acid and ethanol.

USE - The method is used to produce a clear whey protein product. The formula produced from (1) is useful as a nutritional formula in sports drinks, fruit gels, ice cream and cookies, and/or as an infant food. The infant food is non-allergenic (all claimed). The whey products may also be

used for the production of cheese.

DESCRIPTION OF DRAWING(S) - The diagram shows the basic steps in the cheese making process.

Dwg.1/13

FS CPI

FA AB; GI; DCN

MC CPI: A12-M; A12-W11; B04-B04K; B04-L03B; B04-N02; B11-B; D03-B02; D03-B06;
D03-F01; D03-H01T2

TECH UPTX: 20001027

TECHNOLOGY FOCUS - BIOTECHNOLOGY - Preferred Methods: In the method of (1), the steps of eluting **alpha**-lactalbumin, lactoperoxidase, serum albumin and lactoferrin utilize a buffer. The method of (1) further comprises the step of cleaning the 2 resins with a cleaning buffer. The method of (2) further comprises an anion exchange resin and the steps of passing the deproteinized (processed) whey through the anion exchange resin, and eluting the remaining proteins and optionally washing the whey proteins to produce a clear whey isolate. The whey proteins adsorbed onto the cation exchange resin are eluted. The cation exchange resin is washed to produce a wash buffer. The whey protein isolate of (3) comprises immunoglobulins, beta-lactoglobulin, **alpha**-lactalbumin. Adsorbed whey proteins are eluted using a clear whey protein isolate buffer. Serum albumin and lipoproteins are eluted using a serum albumin buffer. The method further comprises ultrafiltering the clear whey protein isolate and diafiltrating the ultrafiltrate. In the method of (4) beta-lactoglobulin is eluted from the anion resin. The method of (5) further comprises equilibrating the cleansed resin. The washed resin is rinsed with water prior to washing with sodium hypochlorite. The base-treated resin is rinsed with water prior to exposing to hydrochloric acid. The acid treated resin is rinsed with water prior to ethanol exposure. The method further comprises passing whey enriched in **alpha**-lactalbumin through a cation exchange resin.

Preferred Whey: The whey is pasteurized sweet whey, pasteurized acid whey, non-pasteurized acid whey, and/or whey protein concentrate. The flow through comprises a formula comprising at least 1 whey protein. The method further comprises diafiltrating the formula. The whey isolate is freeze dried, frozen or is spray dried (to form a powder).

Preferred Container: The container comprises a radial flow column, an axial flow column, or is a beaker, tank, vat or chamber.

Preferred Resin: The cationic exchange resin comprises a cellulose matrix, a co-polymerized glycidyl methacrylate or a cross-linked diethylene glycol. The cationic exchange resin comprises cross-linked flexible sponge absorbent. The cross-linked flexible sponge absorbent comprises substantially uniformly distributed fibrous reinforcement. In the method of (1) the 2 resins are independently reconditioned. In the method of (2) the cation exchange buffer is a weak acid cation exchange resin (preferably a carboxymethyl resin) and the anion exchange resin is a weak base anion exchange resin (preferably a dithylaminoethyl resin). The cation and anion exchange resins are reconditioned with buffers. The anion exchange resin is a radial or axial flow column.

Preferred Buffer: The buffer is selected from whey buffer, permeate and modified whey buffer. The buffer is recycled. The cleaning buffer comprises sodium hydroxide, sodium chloride and ethanol. The wash buffer of (2) comprises non-protein nitrogen. The cation and anion buffers comprise deproteinized whey. The anion buffer comprises lactose, minerals, lactic acid, and vitamins. The clear whey protein isolate buffer of (3) comprises sodium acetate and sodium chloride, the flow-through, (recycled) deproteinized whey or whey buffer. The serum albumin buffer comprises sodium chloride and sodium acetate or sodium citrate salt. Both buffers are recycled.

TI Economical process for isolating beta-lactoglobulin and alpha-lactalbumin in substantially purified state, in single contacting step, in one column, without use of salt for elution.

DC B04 D13

IN ETZEL, M R

PA (WISC) WISCONSIN ALUMNI RES FOUND

CYC 1

PI US 5986063 A 19991116 (200002)* 16p C07K001-18

ADT US 5986063 A US 1998-126904 19980731

PRAI US 1998-126904 19980731

IC ICM C07K001-18

ICS A23J001-20; C07K014-435

AB US 5986063 A UPAB: 20000112

NOVELTY - A process for isolating beta-lactoglobulin and alpha-lactalbumin comprising eluting proteins bound to an ion exchanger using different pH values alone, is new.

DETAILED DESCRIPTION - The process comprises:

(a) adjusting whey protein solution to pH of less than 4.5;

(b) fractionating by contacting with cation exchanger to give bound fraction containing beta-lactoglobulin and alpha-lactalbumin;

(c) adjusting bound fraction to pH of 4-6;

(d) in absence of sodium chloride, eluting at pH of (c) to obtain substantially purified beta-lactoglobulin fraction and remaining fraction on cationic exchanger;

(e) adjusting remaining bound fraction to pH of 6.5 or greater; and

(f) in absence of sodium chloride, eluting at pH of (e) to obtain substantially purified alpha-lactalbumin fraction.

USE - The process is used to isolate beta-lactoglobulin (claimed), which is used as a gelling agent in hams, surimi and other foods, especially in Japan, and to isolate alpha-lactalbumin (claimed), which is used in preparation of humanized milk and compositions of non-allergenic milk for infants allergic to beta-lactoglobulin in cows' milk, as an important food ingredient and a stable emulsifier and foaming agent, e.g. in salad dressings and cake mixes.

ADVANTAGE - Single cation-exchange that produces both proteins in substantially purified state. Isolates both proteins, superior in terms of purity from solution containing whey proteins in single contacting step, in one column, without use of salt for elution. More economical for production of both proteins from single batch of whey.

Dwg.0/9

FS CPI

FA AB; DCN

MC CPI: B04-B04K; B04-N02; B11-C08D2; D03-B; D03-H01J; D03-H01N; D03-H01Q

TECH UPTX: 20000112

TECHNOLOGY FOCUS - ORGANIC CHEMISTRY - Preferred method: Cation exchanger comprises porous membranes containing charged immobilized groups. Process is conducted at 35-50 (about 40) degreesC. In (c), fraction bound to cation exchanger in (b) is adjusted to about pH 4.9. In (e), remaining fraction bound to cation exchanger from (d) is adjusted to about pH 6.5.

ABEX UPTX: 20000112

EXAMPLE - Water-jacketed chromatography column operated at 35 degreesC was packed with sulfopropyl cation exchanger (100 ml). Mozzarella cheese whey was adjusted to pH 3.0 using 1M phosphoric acid and 500 ml was pumped into the column in upflow at flow rate of 8 ml/minute. Ion exchanger was washed with water (180 ml) to remove contaminants, minerals, lactose and fat. Ion exchanger was washed with solution (385 ml) of 0.2M sodium citrate, 0.02M ethylene diaminetetra acetic acid (EDTA) tetra sodium salt, pH 3. Beta-Lactoglobulin was eluted from ion exchanger using 0.2M sodium citrate (1,280 ml; pH 4.9). Alpha-lactalbumin was eluted from ion exchanger using 0.2M sodium citrate, 0.05M calcium chloride (930 ml; pH 6.5).

L114 ANSWER 3 OF 17 WPIX (C) 2003 THOMSON DERWENT
 AN 1999-371026 [31] WPIX
 DNC C1999-109521
 TI An agent for transporting **alpha-lactalbumin** into cancer cells.
 DC B04 D16 K08
 IN HAKANSSON, P A; SVANBORG, C
 PA (HAKA-I) HAKANSSON P A; (SVAN-I) SVANBORG C
 CYC 83
 PI WO 9927967 A1 19990610 (199931)* EN 48p A61K047-48
 RW: AT BE CH CY DE DK EA ES FI FR GB GH GM GR IE IT KE LS LU MC MW NL
 OA PT SD SE SZ UG ZW
 W: AL AM AT AU AZ BA BB BG BR BY CA CH CN CU CZ DE DK EE ES FI GB GE
 GH GM HR HU ID IL IS JP KE KG KP KR KZ LC LK LR LS LT LU LV MD MG
 MK MN MW MX NO NZ PL PT RO RU SD SE SG SI SK SL TJ TM TR TT UA UG
 US UZ VN YU ZW
 AU 9911710 A 19990616 (199945)
 EP 1032426 A1 20000906 (200044) EN A61K047-48
 R: AT BE CH CY DE DK ES FI FR GB GR IE IT LI LU MC NL PT SE
 JP 2001524535 W 20011204 (200203) 48p A61K047-48
 ADT WO 9927967 A1 WO 1998-IB1920 19981123; AU 9911710 A AU 1999-11710
 19981123; EP 1032426 A1 EP 1998-954689 19981123, WO 1998-IB1920 19981123;
 JP 2001524535 W WO 1998-IB1920 19981123, JP 2000-522952 19981123
 FDT AU 9911710 A Based on WO 9927967; EP 1032426 A1 Based on WO 9927967; JP
 2001524535 W Based on WO 9927967
 PRAI GB 1997-25126 19971127
 IC ICM A61K047-48
 ICS A61K009-06; A61K009-08; A61K038-00; A61K039-44; A61K047-42;
 A61K051-00; A61K051-08; A61P035-00
 AB WO 9927967 A UPAB: 19990806
 NOVELTY - An agent (A) comprising a protein complex comprising an oligomeric form of **alpha-lactalbumin** (MAL) and a further reagent (I), which is combined with MAL such that it is carried into the nucleoplasm of cells which are susceptible to MAL.
 DETAILED DESCRIPTION - INDEPENDENT CLAIMS are also included for the following:
 (1) a method of treating cancer which comprises administering to cancer cells, a pharmaceutical composition (A) comprising a carrier or excipient; and
 (2) a method of diagnosing cancer which method comprises applying to cells which are suspected of being cancerous, (A) and observing penetration of the agent into the nucleus of these cells.
 USE - (A) is used in the treatment or in vitro diagnosis of cancer (claimed).
 Dwg.0/0
 FS CPI
 FA AB; DCN
 MC CPI: B04-N02; B12-K04; B14-H01; D05-H09; D05-H11A; K08-X; K09-B
 TECH UPTX: 19990806
 TECHNOLOGY FOCUS - BIOTECHNOLOGY - Preferred materials: (I) is coupled to MAL by conjugation or by covalent bonding. (I) covalently bonded to MAL by way of a linking or spacer group. (I) comprises a polypeptide or protein which is fused to MAL. (I) is selected from cytotoxin, a microbial toxin or an antibody, especially a monoclonal antibody. (I) comprises a labeling agent selected from biotin or a radioactive label, e.g. ^{125}I , ^{14}C or ^{15}S .
 ABEX UPTX: 19990806
 ADMINISTRATION - (A) is made into a solution or cream for topical use. Alternatively, (A) is adapted for oral administration.
 EXAMPLE - To detect intracellular protein, the L1210, A549 and HRTEC cells were fixed at various times after addition of 0.3 mg/ml of biotinylated MAL for 5 minutes in phosphate-buffered para formaldehyde (4%) at room temperature, washed in phosphate buffered saline (PBS), and permeabilized with 0.1% saponin in PBS. FITC conjugated streptavidin (diluted 1:100 in

0.1% saponin) was added and the cells were incubated for 30 minutes at room temperature.

The cells were washed twice in PBS saponin and once in PBS, mounted on a glass slide and analyzed in a Bio-Rad 1024 laser scanning con focal equipment attached to a Nikon Diaphot inverted microscope.

Permeabilization with the saponin allowed entry of streptavidin. Cells treated with medium, biotinylated BSA or α -lactalbumin served as controls. Nuclear uptake of MAL was shown to occur rapidly in cells that were sensitive to its apoptosis-inducing effects. Nuclear staining of L1210 cells was first detected after about 2 hours in about 10% of the cells, and after 6 hours more than 70% of L1210 cell nuclei stained brightly. Cytoplasmic staining was not observed in those cells.

Nuclear localization of MAL in the A549 cells required longer incubation times. About 15% of A549 cell nuclei stained brightly. In the meantime, MAL was observed in the cytoplasm of A549 cells as granular fluorescence evenly distributed throughout the cell. Nuclear uptake was not observed in the HRTEC cells exposed to the biotinylated MAL (1mg/ml). There was a marked difference in the nuclear uptake of ALA compared to MAL. Nuclear staining of ALA was only detected in circa. 30% of L1210 cells after 6 hours and in about 15% OF A549 cells after 24 hours. No staining of ALA was detected in the HRTEC cells.

L114 ANSWER 4 OF 17 WPIX (C) 2003 THOMSON DERWENT
 AN 1999-357815 [30] WPIX
 DNC C1999-105891
 TI Production of oligomeric α -lactalbumin useful for inducing apoptosis in tumor cells.
 DC B04 D16
 IN HAKANSSON, P A; SVANBORG, C; SVENSSON, M W
 PA (HAKA-I) HAKANSSON P A; (SVAN-I) SVANBORG C; (SVEN-I) SVENSSON M W
 CYC 83
 PI WO 9926979 A1 19990603 (199930)* EN 48p C07K014-76 <--
 RW: AT BE CH CY DE DK EA ES FI FR GB GH GM GR IE IT KE LS LU MC MW NL
 OA PT SD SE SZ UG ZW
 W: AL AM AT AU AZ BA BB BG BR BY CA CH CN CU CZ DE DK EE ES FI GB GE
 GH GM HR HU ID IL IS JP KE KG KP KR KZ LC LK LR LS LT LU LV MD MG
 MK MN MW MX NO NZ PL PT RO RU SD SE SG SI SK SL TJ TM TR TT UA UG
 US UZ VN YU ZW
 AU 9912541 A 19990615 (199944)
 EP 1032596 A1 20000906 (200044) EN C07K014-76 <--
 R: AT BE CH CY DE DK ES FI FR GB GR IE IT LI LU MC NL PT SE
 JP 2001524491 W 20011204 (200203) 53p C07K014-76 <--
 ADT WO 9926979 A1 WO 1998-IB1919 19981123; AU 9912541 A AU 1999-12541.
 19981123; EP 1032596 A1 EP 1998-955823 19981123, WO 1998-IB1919 19981123;
 JP 2001524491 W WO 1998-IB1919 19981123, JP 2000-522135 19981123
 FDT AU 9912541 A Based on WO 9926979; EP 1032596 A1 Based on WO 9926979; JP
 2001524491 W Based on WO 9926979
 PRAI GB 1998-12202 19980605; GB 1997-24725 19971121
 IC ICM C07K014-76
 ICS A61K038-00; A61K038-38; A61P031-04; A61P035-00; B01D015-04;
 B01D015-08; B01J041-04
 AB WO 9926979 A UPAB: 19990802
 NOVELTY - A new method (M1) of producing a biologically active oligomeric form of α -lactalbumin (aLA) comprises oligomerising and stabilizing aLA in the molten globule-like state.
 DETAILED DESCRIPTION - INDEPENDENT CLAIMS are also included for the following:
 (1) a method for producing an oligomeric form of aLA which comprises exposing a source of aLA to an ion exchange medium which has been pre-treated with casein or an active component and recovering aLA in an oligomeric form;
 (2) an ion exchange medium for use in the above methods, where the medium has been treated with casein or its active components;

(3) an ion exchange column comprising the ion exchange medium of (2);
and

(4) an oligomeric form of aLA obtained by a method as in (M1) or (1).

USE - The oligomeric aLA is able to induce apoptosis in tumor cells
and/or has a bactericidal effect not seen with monomeric aLA.

Dwg.0/8

FS CPI

FA AB; DCN

MC CPI: B04-C03D; B04-N02; B14-A01; B14-H01; D05-H17A6

TECH UPTX: 19990802

TECHNOLOGY FOCUS - BIOTECHNOLOGY - Preferred Method: The aLA in a molten globule-like state is applied to an anion exchange column which contains a conversion reagent e.g. a component of casein or oleic acid. The column has been eluted with the conversion reagent. The aLA may be subjected to a pretreatment with a calcium chelating agent, e.g. EDTA and low pH, e.g. using HCl, in order to maximize the amount of molten globule-like material. The pre-treatment step comprises heating the aLA to a temperature in excess of from 25-120 degrees Centigrade, preferably 70 degrees Centigrade. The aLA is applied to the column together with a reagent which will induce it to form the molten globule-like state. The molten globule-like inducing reagent is a calcium chelating agent, such as EDTA, present in the elution buffer. The conversion reagent comprises a fatty acid (e.g. oleic acid) or a lipid which is a component of casein. aLA is a mutated form of the native protein in which the calcium binding sites are modified. Particularly the cysteine residues of the aLA are mutated.

In the method of (2), the active component is oleic acid in substantially pure form. The ion exchange medium has been treated with caesin derived from human milk, or caesin which has been previously frozen or is derived from frozen milk. The calcium chelating agent is contacted with aLA prior to contact with the ion exchange medium. The calcium chelating agent is added to an elution buffer which is then used to effect the contact between the aLA and the ion exchange medium. The ion exchange medium comprises EDTA trisacryl. The ion exchange column is eluted with casein or its active components in an ion exchange buffer such as Tris-HCL, followed by elution with a source of aLA (such as monomeric bovine or human aLA) dissolved in the ion exchange buffer in the presence of a salt gradient. The column is washed by elution with the ion exchange buffer twice.

ABEX UPTX: 19990802

EXAMPLE - Oligomeric alpha-lactalbumin (aLA) was prepared using DEAE Trisacryl M and the buffers A: 10mM Tris-HCl pH 8.5, and B: 10mM Tris-HCl with 1M NaCl pH 8.5. 300mg of casein derived from human milk was run on a fresh unused ion exchange matrix. The matrix was then washed with 2 runs of buffer A. Untreated monomeric human aLA (8mg) was added to the column.

2 multimeric peaks were found. 4 further samples were run down this column and all gave 2 multimeric peaks. The 2 peaks which are believed to contain monomeric aLA were kept separately and tested individually using L1210 tumor cells. The results showed that peaks 1 and 2 at 1mg/ml reduced the viability of the tumor cells.

L114 ANSWER 5 OF 17 WPIX (C) 2003 THOMSON DERWENT

AN 1999-254553 [21] WPIX

DNC C1999-074445

TI Continuous chromatographic sequential separation of whey proteins.

DC B04 D13

IN AHMED, S H; MIRANDA, Q; SAXENA, V

PA (SEPR-N) SEPRAGEN CORP

CYC 23

PI WO 9915024 A1 19990401 (199921)* EN 37p A23C009-14

RW: AT BE CH DE DK ES FI FR GB GR IE IT LU MC NL PT SE

W: AU CA JP KR NZ

AU 9745893 A 19990412 (199934)
 EP 1017286 A1 20000712 (200036) EN A23C009-14
 R: AT BE CH DE DK ES FI FR GB GR IE IT LI LU MC NL PT SE
 KR 2001030665 A 20010416 (200163) A23C009-14
 JP 2001516599 W 20011002 (200172) 35p A23C009-14
 NZ 503566 A 20021025 (200274) A23C009-14
 ADT WO 9915024 A1 WO 1997-US16993 19970922; AU 9745893 A AU
 1997-45893 19970922, WO 1997-US16993 19970922; EP 1017286
 A1 EP 1997-944384 19970922, WO 1997-US16993 19970922;
 KR 2001030665 A WO 1997-US16993 19970922, KR 2000-703033
 20000322; JP 2001516599 W WO 1997-US16993 19970922, JP
 2000-512418 19970922; NZ 503566 A NZ 1997-503566 19970922,
 WO 1997-US16993 19970922
 FDT AU 9745893 A Based on WO 9915024; EP 1017286 A1 Based on WO 9915024; JP
 2001516599 W Based on WO 9915024; NZ 503566 A Based on WO 9915024
 PRAI WO 1997-US16993 19970922
 IC ICM A23C009-14
 ICS A23C009-152; A23L001-305; C07K001-16
 AB WO 9915024 A UPAB: 19990603
 NOVELTY - Continuous **chromatographic** sequential separation of whey proteins comprises adsorbing liquid whey on a separation medium packed in a **chromatographic** column and sequentially eluting immunoglobulin, beta-lactoglobulin, **alpha-lactalbumin**, bovine serum albumin and lactoferrin fractions.
 DETAILED DESCRIPTION - INDEPENDENT CLAIMS are also included for the following:
 (1) an infant formula containing at least 25% lactoferrin and less than 0.5 % beta-lactoglobulin;
 (2) an infant formula comprising approx. **a-lactalbumin**, lactoferrin, immunoglobulin and bovine serum albumin and
 (3) a fat substitute comprising 60% approx. **b-lactoglobulin** and 40% approx. **a-lactalbumin**.
 USE - Used for producing infant formula (claimed) and dietary and pharmaceutical formulations.
 ADVANTAGE - The method sequentially and completely separates whey proteins in a one or two step process without denaturation.
 Dwg.0/3
 FS CPI
 FA AB; DCN
 MC CPI: B04-N02; B14-E11; B14-E12; D03-H01T2
 TECH UPTX: 19990603
 TECHNOLOGY FOCUS - BIOLOGY - Preferred process: The liquid whey comprises pasteurized sweet whey, pasteurized or non pasteurized acid whey or whey protein concentrate. The separation medium is a cationic resin. The sequentially eluted immunoglobulin, beta-lactoglobulin, **alpha-lactalbumin**, bovine serum albumin and lactoferrin are further purified by diafiltration. The separation comprises:
 (1) packing a **chromatographic** column with a cationic exchange resin to form a packed **chromatographic** column;
 (2) equilibrating the packed **chromatographic** column;
 (3) passing a whey sample through the packed **chromatographic** column to adsorb the whey proteins to the packed column;
 (4) collecting the flow through from the packed column where the flow comprises lactose, minerals, lactic acid and non-nitrogenous components;
 (5) sequentially eluting the immunoglobulin and beta-lactoglobulin from the packed **chromatographic** column;
 (6) eluting **alpha-lactalbumin** from the packed column;
 (7) reconditioning the packed **chromatographic** column;
 (8) eluting bovine serum albumin and
 (9) eluting lactoferrin from the column.
 Separating beta-lactoglobulin from whey proteins comprises packing a

chromatographic column with an anionic exchange resin, equilibrating it, passing a whey sample through the column to adsorb beta-lactoglobulin, collecting the flow-through comprising **alpha-lactalbumin**, immunoglobulin, bovine serum albumin and lactoferrin and eluting the adsorbed beta-lactoglobulin from the column with a buffer to produce eluate.

The method also comprises packing a second **chromatographic** column with a cationic exchange resin, equilibrating it, passing the flow through a 10000 molecular weight cut off ultrafiltration membrane to produce an ultrafiltrate, passing the ultrafiltrate through the second column to adsorb immunoglobulin, **alpha-lactalbumin**, bovine serum albumin and lactoferrin, eluting the immunoglobulin from the column followed by **alpha-lactalbumin**, reconditioning the column and eluting the bovine serum albumin followed by lactoferrin. The flow-through is combined with the eluate to produce a fat substitute.

TECHNOLOGY FOCUS - FOOD - Preferred Formula: The flow through comprises an infant formula. The infant formula further comprises casein hydrolysate, fat, nonfat milk solids, carbohydrate, minerals and vitamins, vegetable solids and/or sweeteners.

ABEX UPTX: 19990603

EXAMPLE - Commercially whey as a by-product of mozzarella cheese manufacture was clarified to remove casein fines, centrifuged to remove milk fat residue, pasteurized at 162degreesF for 18 seconds and chilled to 40degreesF by passing it through HTST plate heat exchangers. 1 l Of the obtained skimmed commercial sweet whey at pH 6.4 and 6.2% total solids was pH adjusted to 3.8 with acetic acid at 40degreesF. The whey product comprised (in %): total solids (6.2); lactose (4.5); protein (0.8); fat (0.08); ash (0.77) and lactic acid (0.05).

The whey was passed through a 250 ml radial flow **chromatographic** column prepakced with a strong S cation exchange resin and equilibrated with 0.05 M acetate buffer at pH 3.8. All the whey proteins were bound to the resin matrix and the effluent containing non-protein components including lactose, minerals, lactic acid and non-protein nitrogenous components were passed through. The resin with the bound proteins was then washed with 0.05 M acetate buffer at pH 3.8. Immunoglobulin and beta-lactoglobulin were eluted with a buffer at pH 4.0 containing 0.1 M sodium acetate and 0.5 M sodium chloride.

The column was reconditioned and equilibrated with 0.05 M acetate buffer at pH 4.0. **alpha-Lactalbumin** fraction was eluted with a pH 5.0 buffer containing 0.1 M sodium acetate and 0.1 M sodium chloride.

The column was again reconditioned with a pH 5.0 buffer containing 0.05M sodium acetate. Bovine serum albumin was then eluted with a 0.05 M phosphate buffer at pH 7.0 followed by elution of lactoferrin at pH 7.5 with a buffer containing 0.05 M sodium phosphate and 0.5 M sodium chloride.

The column was regenerated by washing it with a solution containing 0.2 M sodium hydroxide and 1 M sodium chloride followed by washing with 20% ethanol solution to sterilize the column and equilibrate with acetate buffer at pH 3.8 for reuse.

L114 ANSWER 6 OF 17 WPIX (C) 2003 THOMSON DERWENT

AN 1998-414731 [36] WPIX

DNC C1998-125238

TI Treating cancer comprises administering multimeric **alpha-lactalbumin** - by injection or as controlled release implant, without adverse effects on lymphoid cells.

DC B04

IN HAKANSSON, A; SABHARWAL, H; SVANBORG, C

PA (HAKA-I) HAKANSSON A; (SABH-I) SABHARWAL H; (SVAN-I) SVANBORG C

CYC 1

PI CA 2188903 A 19980425 (199836)* EN 34p A61K038-38 <--

ADT CA 2188903 A CA 1996-2188903 19961025

PRAI CA 1996-2188903 19961025

IC ICM A61K038-38

AB CA 2188903 A UPAB: 19980911

Treatment of cancer in a mammal comprises administration of multimeric alpha-lactalbumin (MLA). Also claimed are: (a) a sterile aqueous solution of MLA; (b) a sterile injectable composition for use in the treatment of cancer in mammals, comprising MLA in a pharmaceutical diluent; (c) extracorporeal treatment of human body fluids, by adding sufficient MLA to kill all of any cancer cells in the fluid; (d) a composition comprising an extracorporeal human body fluid containing sufficient MLA to kill all of any cancer cells in the fluid; (e) the use of MLA in the preparation of a sterile injectable composition for use in cancer therapy; and (f) a sterile composition comprising a solid containing MLA for insertion into a mammalian body to act as a controlled release source of MLA.

USE - MLA is an anticancer agent which induces apoptosis in transformed cells. It is active against cancers in low differentiated cells such as epithelial cells (e.g. lung, bronchial, kidney, bladder, mammary and small intestinal cells) and non-epithelial cells such as fibroblast cells (connective tissue).

ADVANTAGE - Any adverse effects of MLA on lymphoid cells are acceptably low in in vivo tests.

Dwg:0/4

FS CPI

FA AB

MC CPI: B04-B04L; B04-N02; B12-M10; B14-H01

L114 ANSWER 7 OF 17 WPIX (C) 2003 THOMSON DERWENT

AN 1998-321630 [28] WPIX

DNC C1998-098922

TI Process for sequential chromatographic separation of whey proteins - using radial flow chromatography, for use in e.g. infant feeding formulas.

DC B04 D13

IN AHMED, S H; MIRANDA, Q R; MOZAFFAR, Z; SAXENA, V

PA (SEPR-N) SEPRAGEN CORP

CYC 1

PI US 5756680 A 19980526 (199828)* 13p C07K016-04 <--

ADT US 5756680 A Cont of US 1994-177574 19940105, US

1996-678364 19960716

PRAI US 1994-177574 19940105; US 1996-678364 19960716

IC ICM C07K016-04

ICS A23C009-14; C07K001-36; C07K014-47

AB US 5756680 A UPAB: 19980715

A process of continuous sequential separation of whey proteins (i.e. lactoferrin (LF), immunoglobulin (IgG), lactoglobulin (Lg), - lactalbumin (La) and bovine serum albumin (BSA)) comprises passing the liquid whey through a chromatographic column packed with cationic ion exchange resin, and sequentially eluting the proteins with suitable buffers, reconditioning the column as necessary, to obtain IgG and Lg, then La, then BSA, then LF. Also claimed is a method of separating Lg from whey proteins comprising: (1) passing the whey sample through a radial flow chromatographic column packed with an ionic exchange resin, where Lg is adsorbed; (2) collecting the permeate comprising other proteins (listed above); (3) eluting Lg with buffer; (4) passing the permeate from (3) through an ultrafiltration membrane, and (5) passing the ultrafiltrate through a second chromatographic column, from which the proteins can be sequentially eluted as described above.

USE - Proteins can be separated from pasteurised sweet whey, pasteurised or non-pasteurised acid whey, and whey protein concentrate. The separated proteins are used in pharmaceutical and dietary formulations, particularly infant feeding formulas (see 'Preferred

Compositions').

Dwg.0/3

FS CPI

FA AB

MC CPI: B04-N02; B11-B; B14-E11; D03-F01; D03-F04; D03-F05; D03-F06;
D03-H01T2

L114 ANSWER 8 OF 17 WPIX (C) 2003 THOMSON DERWENT
AN 1998-008482 [01] WPIX

DNC C1998-002948

TI Separating a soluble milk component from milk - by tangential flow filtration to produce permeate containing the component and using capture device for the component.

DC B04 D13

IN HAYES, M L; KUTZKO, J P; SHERMAN, L T

PA (GENZ) GENZYME TRANSGENICS CORP

CYC 23

PI WO 9742835 A1 19971120 (199801)* EN 29p A23J001-20 <--
RW: AT BE CH DE DK ES FI FR GB GR IE IT LU MC NL PT SE

W: AU CA JP NZ US

AU 9729402 A 19971205 (199814) A23J001-20 <--

EP 923308 A1 19990623 (199929) EN A23J001-20 <--

R: AT BE CH DE DK ES FI FR GB GR IE IT LI LU MC NL PT SE

NZ 332916 A 20000526 (200033) A23J001-20

JP 2000510701 W 20000822 (200045) 33p C12N015-09

AU 725993 B 20001026 (200059) A23J001-20

US 6268487 B1 20010731 (200146) C07K001-14

EP 923308 B1 20020918 (200269) EN A23J001-20 <--

R: AT BE CH DE DK ES FI FR GB GR IE IT LI LU MC NL PT SE

DE 69715641 E 20021024 (200278) A23J001-20

ADT WO 9742835 A1 WO 1997-US8044 19970513; AU 9729402 A AU

1997-29402 19970513; EP 923308 A1 EP 1997-923643 19970513,

WO 1997-US8044 19970513; NZ 332916 A NZ 1997-332916

19970513, WO 1997-US8044 19970513; JP 2000510701 W JP

1997-541036 19970513, WO 1997-US8044 19970513; AU 725993 B

AU 1997-29402 19970513; US 6268487 B1 US 1996-648235

19960513; EP 923308 B1 EP 1997-923643 19970513, WO

1997-US8044 19970513; DE 69715641 E DE 1997-615641 19970513

, EP 1997-923643 19970513, WO 1997-US8044 19970513

FDT AU 9729402 A Based on WO 9742835; EP 923308 A1 Based on WO 9742835; NZ 332916 A Based on WO 9742835; JP 2000510701 W Based on WO 9742835; AU 725993 B Previous Publ. AU 9729402, Based on WO 9742835; EP 923308 B1 Based on WO 9742835; DE 69715641 E Based on EP 923308, Based on WO 9742835

PRAI US 1996-648235 19960513

IC ICM A23J001-20; C07K001-14; C12N015-09

ICS A01K067-027; A23C009-142; A23C009-146; C07K001-16; C07K001-18; C07K001-22; C12N005-10

AB WO 9742835 A UPAB: 19980107

Separation of a soluble milk component (SMC) from milk or a milk fraction, comprises: (a) subjecting the milk or milk fraction to tangential flow filtration across a membrane of sufficient porosity to form a retentate and a permeate comprising the SMC; (b) subjecting the permeate to a capture device to remove the SMC; (c) combining the effluent from the capture device in step (b) with the original milk sample, and (d) repeating steps (a)-(c) until the SMC is recovered.

The tangential flow filter has a pore size 0.1-1000 nm. The milk may be combined with a chelating agent, e.g. EDTA, EGTA or citrate added to a final concentration 1-500 mM. The capture device may be an affinity chromatography capture device, such as a heparin column, a Protein A column or a Protein G column. It is especially an ion exchange chromatography capture device. The milk is obtained from a lactating non-human mammal selected from the group comprising transgenic mammals and transomic mammals.

USE - The method can be used for the separation of SMCs such as glycoproteins, immunoglobulins, peptides, hormones, enzymes, serum proteins, milk proteins, cellular proteins, soluble receptors and industrial enzymes. In particular they can be used for separation of erythropoietin, alpha -1 proteinase inhibitor, alkaline phosphatase, angiogenin, antithrombin III, chitinase, extracellular superoxide dismutase, Factor VIII, Factor IX, Factor X, fibrinogen, glucocerebrosidase, glutamate decarboxylase, human serum albumin, insulin, myelin basic protein, lactoferrin, lactoglobulin, lysozyme, **lactalbumin**, proinsulin, soluble CD4, component and complexes of soluble CD4 or tissue plasminogen activator. The method substantially removes bacteria, mycoplasma, viruses, prion particles and other microbial contaminants present in the raw milk.

ADVANTAGE - The method can provide for the isolation of SMCs in a biologically active form without prior processing to remove fats, lipids, casein micelles or particular matter.

Dwg.0/4

FS CPI
FA AB; DCN
MC CPI: B04-B04K; B11-B; D03-B

L114 ANSWER 9 OF 17 WPIX (C) 2003 THOMSON DERWENT
 AN 1996-139457 [14] WPIX
 DNC C1996-043792
 TI Multi-meric **alpha-lactalbumin** used therapeutically or prophylactically - to treat bacterial infections of the respiratory tract, specifically of *S. pneumoniae* or *H. influenzae*.
 DC B04
 IN SABHARWAL, H; SVANBORG, C
 PA (SABH-I) SABHARWAL H; (SVAN-I) SVANBORG C
 CYC 32
 PI WO 9604929 A1 19960222 (199614)* EN 31p A61K038-38 <--
 RW: AT BE CH DE DK ES FR GB GR IE IT LU MC NL PT SE
 W: AU BR CA CZ FI HU JP KR NO NZ PL RU SK US
 AU 9477922 A 19960307 (199624) A61K038-38 <--
 EP 776214 A1 19970604 (199727) EN A61K038-38 <--
 R: AT BE CH DE DK ES FR GB GR IE IT LI LU NL PT SE
 JP 10504547 W 19980506 (199828) 35p A61K038-00
 EP 776214 B1 19990728 (199934) EN A61K038-38 <--
 R: AT BE CH DE DK ES FR GB GR IE IT LI LU NL PT SE
 DE 69419782 E 19990902 (199942) A61K038-38 <--
 ES 2136206 T3 19991116 (200001)# A61K038-38 <--
 MX 9406245 A1 19990101 (200051)# C07K003-00
 ADT WO 9604929 A1 WO 1994-SE742 19940816; AU 9477922 A AU 1994-77922 19940816,
 WO 1994-SE742 19940816; EP 776214 A1 EP 1994-928519 19940816, WO
 1994-SE742 19940816; JP 10504547 W WO 1994-SE742 19940816, JP 1996-507224
 19940816; EP 776214 B1 EP 1994-928519 19940816, WO 1994-SE742 19940816; DE
 69419782 E DE 1994-619782 19940816, EP 1994-928519 19940816, WO 1994-SE742
 19940816; ES 2136206 T3 EP 1994-928519 19940816; MX 9406245 A1 MX
 1994-6245 19940816
 FDT AU 9477922 A Based on WO 9604929; EP 776214 A1 Based on WO 9604929; JP
 10504547 W Based on WO 9604929; EP 776214 B1 Based on WO 9604929; DE
 69419782 E Based on EP 776214, Based on WO 9604929; ES 2136206 T3 Based on
 EP 776214
 PRAI WO 1994-SE742 19940816; MX 1994-6245 19940816
 REP 02Jnl.Ref; EP 22696; EP 339656; FR 2671697; US 5290571
 IC ICM A61K038-00; A61K038-38; C07K003-00
 ICS A23L003-3526; A61K035-20; G01N033-569
 ICA C07K014-76
 AB WO 9604929 A UPAB: 19960405
 New use of a multimeric **alpha-lactalbumin** (L) in the
 prepn. of therapeutically and/or prophylactically active antibacterial
 preps. against bacteria, particularly *S. pneumoniae* and/or *H. influenzae*.

Also claimed are (i) the method of using (L) for prophylactic and therapeutic purposes, (ii) a method of preparing antibacterial prepsn. contg. (L).

USE - (L) may be used to treat or prevent infections, esp. in the gastrointestinal or respiratory tracts by *S. pneumoniae* and/or *H. influenzae* (claimed) such as otitis media by preventing adhesion and thus colonisation. (L) may be administered as a nasal spray, in tablet or capsule form in conjunction with a carrier, injection or liquid form for oral administration. The nasal spray could be used for prophylactic purposes. (L) may be added to feedstuffs or food (claimed) such as infant food or animal feedstuffs. It may also be used to diagnose infections caused by *S. pneumoniae* and/or *H. influenzae* by determining the degree of interaction between bacterium in a sample and (L).

ADVANTAGE - This new form of (L) could be used as a bactericide on *S. pneumoniae* resistant to antibiotics.

Dwg.0/4

FS CPI
FA AB
MC CPI: B04-N02; B12-K04A4; B14-A01; B14-K01

L114 ANSWER 10 OF 17 WPIX (C) 2003 THOMSON DERWENT

AN 1995-307083 [40] WPIX

DNC C1995-136568

TI Prepn of milk, whey derived beta lacto-globulin and ***alpha-lactalbumin***, etc - comprises adjusting milk whey pH, protein concn and salt concn, contracting with hydrophobic **chromatographic** resin and fractionating.

DC D13

PA (KYOD) KYODO NYUGYO KK

CYC 1

PI JP 07203863 A 19950808 (199540)* 4p A23J001-20 <--

ADT JP 07203863 A JP 1994-14964 19940114

PRAI JP 1994-14964 19940114

IC ICM A23J001-20

ICS C07K001-20; C07K014-47

AB JP 07203863 A UPAB: 19951011

Prepn. of milk whey-derived beta-lactoglobulin, ***alpha-lactoalbumin***, and lactoferrin comprises (a) adjusting milk whey to pH 4.4-4.6, a protein concn. of 0.5-10%, and NaCl concn. of 1.0M, (B) contacting the milk whey with a hydrophobic **chromatographic** resin; and (c) fractionating the milk whey with 0.75 M NaCl and 40% (V/V) ethanol.

ADVANTAGE - The functional gp. of the hydrophobic **chromatographic** resin is a butyl or phenyl gp., and has improved acid resistance, base resistance, pressure resistance, and microorganism resistance, and is used at room temp. The method reduces prices for beta-lactoglobulin, ***alpha-lactalbumin***, and lactoferrin as food ingredients. The final prod. has no nonreversible deterioration. The method efficiently produces each protein in a series of processes.

Dwg.0/3

FS CPI

FA AB

MC CPI: D03-B; D03-F01

L114 ANSWER 11 OF 17 WPIX (C) 2003 THOMSON DERWENT

AN 1995-269223 [35] WPIX

DNC C1995-122031

TI Fractionating whey or whey protein soln. chromatographically - comprises clarifying soln. and removing glyco-macro-peptide(s), and passing soln. through chromatography column packed with anion exchange resin.

DC D13

IN ANTILA, P; HARJU, M; OUTINEN, M; TOSSAVAINEN, O

PA (VALI-N) VALIO OY; (VALI-N) VALIO LTD

CYC 7
 PI WO 9519714 A1 19950727 (199535)* EN 23p A23J001-20
 FI 9400316 A 19950722 (199542) A23J001-20
 AU 9514193 A 19950808 (199545) A23J001-20
 FI 96090 B 19960131 (199609) A23J001-20
 EP 757522 A1 19970212 (199712) EN A23J001-20
 R: DE DK FR IE NL
 ADT WO 9519714 A1 WO 1995-FI27 19950120; FI 9400316 A FI 1994-316 19940121; AU 9514193 A AU 1995-14193 19950120; FI 96090 B FI 1994-316 19940121; EP 757522 A1 EP 1995-905668 19950120, WO 1995-FI27 19950120
 FDT AU 9514193 A Based on WO 9519714; FI 96090 B Previous Publ. FI 9400316; EP 757522 A1 Based on WO 9519714
 PRAI FI 1994-316 19940121
 REP 2.Jnl.Ref
 IC ICM A23J001-20
 ICS A23C009-146; A23C021-00; A23J003-08
 AB WO 9519714 A UPAB: 19950905
 Fractionating whey or whey protein soln. chromatographically into an alpha-lactalbumin and a beta-lactalbumin component comprises (a) clarifying a batch of whey or whey protein soln. and opt. removing glycomacopeptides from it ; (b) passing the soln. through a chromatography column packed with a strong polystyrene-based anion exchange resin and recovering the fraction leaving the column; (c) washing the column with deionised water, the wash water being combined with the above fraction to give the alpha-lactalbumin component; and (d) eluting the washed column with a weak aq. NaCl soln. and recovering the eluate as a beta-lactalbumin component. The resin has a pore size of 1000-2000angstrom and a pore vol. of 0.9 cm³/g and in which a quat. alkyl amine or alkyl alkanolamine gp. (esp. alkylalkanolamine gps.) are attached to a styrene-divinyl-benzene-polymer matrix. The resin has a particle dia. of 300-600 mum. Also claimed are the obtd. alpha- and beta-lactalbumin components.

USE - The alpha- and beta-lactalbumins are useful in infant food formulas and as protein component in food industry respectively, in clinical nutritive preps. and various prods. in the food industry.

ADVANTAGE - The process is useful for fractionating proteins from different types of whey. The resin used for the sepn. is cheaper than prior art resins. The process allows most of the beta-lactalbumins to be sepd. from native whey into a fraction free of other whey proteins at pH 6-7.

Dwg.1/2

FS CPI
 FA AB; GI
 MC CPI: D03-B; D03-F01

L114 ANSWER 12 OF 17 WPIX (C) 2003 THOMSON DERWENT
 AN 1994-210011 [26] WPIX
 DNC C1994-095994
 TI Prodn. of whey protein concentrate - enriched in alpha-lactalbumin and/or beta-lactoglobulin, by destabilising lactalbumin in whey protein product before fractionation.

DC D13
 IN BRONTS, H; DE, WIT J N
 PA (CAMP-N) CAMPINA MELKUNIE BV; (DWIT-I) DE WIT J N
 CYC 22
 PI EP 604684 A1 19940706 (199426)* EN 14p A23J001-20 <--
 R: AT BE CH DE DK ES FR GB GR IE IT LI LU MC NL PT SE
 AU 9352674 A 19940707 (199431) A23C009-146 <--
 CA 2111668 A 19940624 (199433) A23J001-20 <--
 NZ 250400 A 19950427 (199522) A23C021-00 <--
 US 5420249 A 19950530 (199527) 12p C07K003-28 <--
 JP 07123927 A 19950516 (199528) 9p A23J001-20 <--
 AU 664934 B 19951207 (199605) A23C009-146 <--

EP 604684 B1 19970611 (199728) EN 14p A23J001-20 <--
 R: AT CH DE DK FR GB GR IE IT LI NL SE
 DE 69220374 E 19970717 (199734) A23J001-20 <--
 ADT EP 604684 A1 EP 1992-204074 19921223; AU 9352674 A AU
 1993-52674 19931223; CA 2111668 A CA 1993-2111668 19931216;
 NZ 250400 A NZ 1993-250400 19931209; US 5420249 A US
 1993-170497 19931220; JP 07123927 A JP 1993-354797 19931222
 ; AU 664934 B AU 1993-52674 19931223; EP 604684 B1 EP
 1992-204074 19921223; DE 69220374 E DE 1992-620374 19921223
 , EP 1992-204074 19921223
 FDT AU 664934 B Previous Publ. AU 9352674; DE 69220374 E Based on EP 604684
 PRAI EP 1992-204074 19921223
 REP EP 16292; EP 38732; FR 2345939; US 2595459; US 2765232; 3.Jnl.Ref
 IC ICM A23C009-146; A23C021-00; A23J001-20; C07K003-28
 ICS A23C009-14; A23J003-08; A23L001-305; A61K035-20; C07K001-14;
 C07K003-12; C07K014-47; C07K015-06
 ICA A61K038-16
 AB EP 604684 A UPAB: 19940817
 Prodn. of whey protein concentrate (A) comprises (1) incubating a soln. of whey protein product (B) with a Ca-binding **ion-exchange** resin in acid form to initiate destabilisation of (I); (2) adjusting pH of the treated soln. to 4.3-4.8 (after sepn. from the resin); (3) incubating at 10-50 deg.C to flocculate (I); (4) fractionating proteins in the soln. phase at pH 4.3-4.8 to give separate fractions enriched in (I) and (II); (5) increasing the pH of the (I)-enriched fraction to solubilise it; (6) opt. increasing the pH of the (II)-enriched fraction to neutralise it.
 Pref. (B) contains 0.7-15% protein, is defatted and has pH at least 5.
 USE/ADVANTAGE - (A) is used in prodn. of humanised and non-allergenic milk products. By pretreating (B) before fractionation, the (I):(II) ratio can be improved and controlled (at any ratio 0.1-10) and minimal waste streams are generated. (I) and (II) are recovered in undenatured form and sepn. is not affected by entrapment of (II) in aggregates of (I).
 Dwg.2/5
 FS CPI
 FA AB
 MC CPI: D03-B07; D03-F01
 ABEQ US 5420249 A UPAB: 19950712
 Alpha-lactalbumin and beta-lactoglobulins are selectively fractionated to recover either protein-enriched whey protein concentrate from an initial whey protein prod..
 Process comprises (a) incubating a soln. contg. whey protein prod. with a calcium-binding ionic exchange resin in acid form to initiate instability of alpha-lactalbumin; (b) adjusting to pH4.3-4.8; (c) incubating at 10-50 deg.C to promote flocculation of alpha-lactalbumin; (d) fractionating proteins at pH4.3-4.8 to form 2 fractions each enriched with corresp. protein; (e) raising pH of the alpha-lactalbumin enriched fraction to solubilise it; and (f) opt. raising the pH of the beta-lactoglobulin enriched fraction to neutralise it.
 USE/ADVANTAGE - The alpha-lactalbumin is useful in non-allergenic infant milk products. Undenatured protein prods. contg. alpha-lactalbumin and beta-lactoglobulin are obtd. in any desired ratio between 0.1-10.
 Dwg.0/5
 ABEQ EP 604684 B UPAB: 19970709
 A process for the recovery of alpha-lactalbumin and/or beta-lactoglobulin enriched whey protein concentrate from a whey protein product, characterised by: a) incubating a solution comprising said whey protein product with a calcium-binding ionic exchange resin in its acid form to initiate the instability of alpha-lactalbumin, b) adjusting the pH of the treated protein product solution to a value between 4.3 and 4.8, after separation of said resin,

c) incubating said protein product solution at a temperature, between 10 and 50 deg. C to promote the flocculation of **alpha-lactalbumin**, d) fractioning the proteins in said protein product solution a pH 4.3-4.8, providing an **alpha-lactalbumin** enriched fraction and a beta-lactoglobulin enriched fraction. e) raising the pH of the **alpha-lactalbumin** enriched fraction sufficiently to solubilise the **alpha-lactalbumin** fraction, and f) optionally raising the pH of the beta-lactoglobulin enriched fraction sufficiently to neutralise the beta-lactoglobulin fraction.

Dwg.0/5

L114 ANSWER 13 OF 17 WPIX (C) 2003 THOMSON DERWENT
 AN 1993-058722 [07] WPIX
 TI **Ion-exchange** membrane for sepn. of charged proteins - provides prods. from biological fluids, e.g. antibodies, vitamin(s), hormones, enzymes, clotting factors, immunoglobulin(s), etc..
 DC B04 C03 D13 D16
 IN DIONYSIUS, D A; GRIEVE, P A; JAMES, E A; MITCHELL, I R; REGESTER, G O; SMITHERS, G W; SMITHERS, G
 PA (CSIR) COMMONWEALTH SCI & IND RES ORG; (DAIR-N) DAIRY RES & DEV CORP; (QUEE-N) STATE QUEENSLAND DEPT PRIMARY IND
 CYC 19
 PI WO 9302098 A1 19930204 (199307)* EN 58p C07K003-22 <--
 RW: AT BE CH DE DK ES FR GB GR IT LU MC NL SE
 W: AU JP US
 AU 9223762 A 19930223 (199324) C07K003-22 <--
 EP 595993 A1 19940511 (199419) EN C07K003-22 <--
 R: AT BE CH DE DK ES FR GB GR IT LI LU MC NL SE
 JP 07502016 W 19950302 (199517) C07K001-18 <--
 NZ 243727 A 19950328 (199519) B01J047-12 <--
 EP 595993 A4 19940817 (199533) C07K003-22 <--
 ADT WO 9302098 A1 WO 1992-AU381 19920724; AU 9223762 A AU 1992-23762 19920724; EP 595993 A1 EP 1992-916550 19920724, WO 1992-AU381 19920724; JP 07502016 W WO 1992-AU381 19920724, JP 1993-502493 19920724; NZ 243727 A NZ 1992-243727 19920727; EP 595993 A4 EP 1992-916550
 FDT AU 9223762 A Based on WO 9302098; EP 595993 A1 Based on WO 9302098; JP 07502016 W Based on WO 9302098
 PRAI AU 1991-7436 19910725
 REP 7.Jnl.Ref; AU 8827180; BE 901672; FR 2487642; FR 2613725; GB 2179947; WO 8910064; No-Citns.
 IC ICM B01J047-12; C07K001-18; C07K003-22
 ICS A23C009-146; A23J001-06; A23J001-20; B01D015-04; B01D061-00; C07K014-575; C07K015-06; C12N009-08
 AB WO 9302098 A UPAB: 19931119
 Process for sepn. of charged molecules from a fluid, comprising: (a) providing an **ion exchange** medium disposed on a porous membrane, pref. with pore size 0.1 to 1.2 microns; (b) passing the fluid through the membrane, so that the charged materials are preferentially adsorbed on the medium; and (c) eluting the adsorbed molecules; is new.
 USE/ADVANTAGE - The process is partic. suitable for treatment of biological fluids, including milk or milk prods., blood or blood plasma, or fermentation or cell culture fluids, and large vols. can be effectively filtered in a single step operation to isolate minor charged components in good yield. The milk prods. include skim milk and whey, the latter considered usually a waste prod. in the dairy industry; also colostrum. Types of molecules which can be isolated include proteins, hormones, vitamins, enzymes, clotting factors, immunoglobulins, peptides,, lysozyme, and antibodies. From milk, lactoferrin, lactoperoxidase, growth promoting agents, glycomacropeptides lysozyme, and **alpha-lactalbumin**; and from blood, clotting factors, serum albumin and immunoglobulins, all prods. of value in both human and veterinary

medicine, are obtd. The effluent from the sepn. may also be of value; e.g. whey effluent, free of particulates and microorganisms, can be processed into a low-fat whey protein concentrate powder with high solubility after extn. of lactoferrin and lactoperoxidase. Use of the membrane avoids traditional ion-exchange column problems of swelling on packing, and maintenance is easier. Fat globules and proteinaceous aggregates which would clog traditional columns are prevented from passing through the porous membrane and are retained on the retentate side, as the pore size is sufficiently small. Elution of the charged molecules can take place either before removal of the aggregates or after (e.g. by means of a wash prior to elution of prods.) rea

Dwg. 1/24

FS CPI
 FA AB; GI
 MC CPI: B04-B02C2; C04-B02C2; B04-B04A6; C04-B04A6; B11-B; C11-B; D05-H13

L114 ANSWER 14 OF 17 WPIX (C) 2003 THOMSON DERWENT

AN 1992-310264 [38] WPIX

DNC C1992-137760

TI Compsn. rich in **alpha lactalbumin** - are prep'd. treating whey with an **ion exchange resin**, and concentrating and/or desalinating.

DC B04 D13

IN MATSUNO, I; NAKANO, T; SHIMATANI, M; SUGAWARA, M; UCHIDA, Y
 PA (SNOW) SNOW BRAND MILK PROD CO LTD

CYC 4

PI	FR 2671697	A1 19920724 (199238)*	13p	A23C021-00	<--
	JP 04330252	A 19921118 (199302)	4p	A23J001-20	<--
	NZ 241328	A 19931125 (199350)		C07K003-22	<--
	US 5434250	A 19950718 (199534)	4p	C07K015-14	<--
	JP 2961625	B2 19991012 (199948)	4p	A23J001-20	

ADT FR 2671697 A1 FR 1992-545 19920120; JP 04330252 A JP 1991-19114 19910121; NZ 241328 A NZ 1992-241328 19920117; US 5434250 A Cont of US 1992-820369 19920114, US 1994-231984 19940421; JP 2961625 B2 JP 1991-19114 19910121

FDT JP 2961625 B2 Previous Publ. JP 04330252

PRAI JP 1991-19114 19910121

IC ICM A23C021-00; A23J001-20; C07K003-22; C07K015-14
 ICS A23C001-14; A23C009-146; A61K039-395; C07K003-24; C07K003-26; C07K003-28

ICA A61K037-02; A61K037-04; A61K038-16; C07K001-34; C07K001-36

AB FR 2671697 A UPAB: 19931113

Compsns. high in **alpha lactalbumin** are prep'd. by either of the following processes: (A) a) cheese whey, acid casein whey, or pressure casein whey is adjusted to pH 5 or more; b) the prod. is contacted with an **anion exchange resin** to give an **ion exchanged** soln.; c) the pH is adjusted to 4 or less; d) the soln. is concentrated and/or desalinated.

(B) a) the same starting material as above is adjusted to pH 2-4; b) it is contacted with a cation exchange resin; steps c) and d) are the same as described above. Pref. the material from stage b) is conc. and crystallised to eliminate lactose. The liquor may then be diluted prior to stage c). The desalination stage d) is pref. effected using an ultrafiltration membrane having a mol. mass exclusion size of 10,000-50,000 daltons. Desiccation in stage d) may be effected by drying to a powder.

USE/ADVANTAGE - The product is useful in foodstuffs and medicines. The described processes are cheap and easy to carry out on an industrial scale

Dwg.0/0

FS CPI

FA AB

MC CPI: B04-B04A6; D03-B; D03-F

ABEQ US 5434250 A UPAB: 19950904

Process for concentrating **lactalbumin** from cheese whey, acid casein whey or rennet casein whey comprises adjusting to pH 5 or higher, contacting with **anion exchanger** and adjusting the **exchanger-passed** soln. to pH 4 or lower, then subjecting to ultrafiltration or diafiltration with membrane having MW cut-off of 10000-50000 to separate the **alpha-lactalbumin** from k-casein glycomacropeptide. Pref. a further concn. and crystallising step of the **exchanger-passed** soln. removes lactose and yields a mother liq. which may be diluted and recycled. **Exchange-passed** soln. may be dried to powder.

USE - Low cost mfr. of high **alpha-lactalbumin** content compsn. for use in food materials and medical materials free of beta-lactalbumin which is an allergen using biprods. from cheese mfr.

Dwg.0/0

L114 ANSWER 15 OF 17 WPIX (C) 2003 THOMSON DERWENT

AN 1987-016118 [03] WPIX

DNC C1987-006611

TI **Alpha-lactalbumin** recovery from whey - by selective thermal pptn..

DC D13

IN BARTHIER, J P; RIALLAND, J P; BARBIER, J; RIALLAND, J

PA (LAIT-N) LAITERIES BRIDEL SA E

CYC 13

PI EP 209414 A 19870121 (198703)* FR 8p <--

R: BE CH DE FR GB IT LI LU NL

FR 2583267 A 19861219 (198704) <--

AU 8658876 A 19861224 (198706) <--

US 4782138 A 19881101 (198846) 5p <--

EP 209414 B 19890830 (198935) FR <--

R: BE CH DE FR GB IT LI LU NL

DE 3665248 G 19891005 (198941) <--

US 4782138 B 19920922 (199241) 3p A23J001-20 <--

EP 209414 B2 19931118 (199346) FR 9p A23J001-20 <--

R: BE CH DE FR GB IT LI LU NL

CA 1328950 C 19940426 (199422) C07K015-06 <--

ADT EP 209414 A EP 1986-401243 19860610; FR 2583267 A FR
1985-9153 19850617; US 4782138 A US 1986-876491 19860617;
US 4782138 B US 1986-876491 19860617; EP 209414 B2 EP
1986-401243 19860610; CA 1328950 C CA 1986-511672 19860616

PRAI FR 1985-9153 19850617

REP 2.Jnl.Ref; DE 2155696; GB 1313085

IC ICM A23J001-20

ICS C07K003-24; C07K015-06

AB EP 209414 A UPAB: 19930922

Sepn. of **alpha-lactalbumin** (I) from whey proteins is effected by concentrating whey to a solids content of 10-40 wt.%, acidifying to a pH below 4, heating at up to 75 deg.C for 0.25-60 min., and recovering the pptd. (I).

USE/ADVANTAGE - (I) is useful as a component of substitute human milk and non-allergenic milk prods. The process avoids use of expensive ion-exchange chromatography equipment.

0/1

FS CPI

FA AB

MC CPI: D03-F01

ABEQ EP 209414 B UPAB: 19940103

Process for selectively separating the **alpha-lactalbumin** from the proteins of whey, characterised in that it comprises a heat treatment of the whey previously concentrated to a dry matter content of 10 to 40% by weight and acidified to a pH less than 4; said heat treatment

being carried out at a temperature of 45 to 60 deg C for a duration of 1 minute to 1 hour or at a temperature of 60 to 75 deg C for a duration of 15 seconds to 1 minute, so as to selectively precipitate the **alpha-lactalbumin**; said heat treatment being followed by the recovery of the **alpha-lactalbumin** in the form of a precipitate and possibly the recovery of the other lacto-proteins remaining in solution in a residual whey.

Dwg.0/1

ABEQ US 4782138 A UPAB: 19930922

Alpha-lactalbumin is selectively sepd. from proteins of whey by (a) heat treating whey conc. to dry matter content of 10-40 wt.% and acidified to less than pH 4 to selectively ppte. **lactalbumin**; the (b) recovering prod. from whey. Heat treatment is at 75 deg. C or less for 15-3600 secs. Pref. whey is conc. by reverse osmosis to dry matter content 25 wt.% or less. Acidification comprises ion exchange using a cation exchange resin in (H⁺)-form.

ADVANTAGE - Method is simple to carry out and has low cost.

ABEQ US 4782138 B UPAB: 19930922

Process for selectively sepg. the **alpha-lactalbumin** from the proteins of whey comprises a heat treatment of the whey previously conc. to a dry matter content of 10-40 wt.%, and acidified to a pH of less than 4, pref. from 3-3.5. The heat treatment being carried out at a temp. not exceeding 75 deg. C., pref. from 45-75 deg. C., for a duration of 15 seconds to 1 hours so as selectively to ppte. the **alpha-lactalbumin**. This heat treatment is followed by the recovery of **alpha-lactalbumin** in the form of a ppte. and possibly of the other lacto-proteins remaining in soln. in the residual whey. The process is simple to carry out and is of low cost.

Claims 5-7 are cancelled

0/0

L114 ANSWER 16 OF 17 WPIX (C) 2003 THOMSON DERWENT

AN 1984-199125 [32] WPIX

DNC C1984-083877

TI Water soluble casein and whey protein ppte. from milk prods. - by adjusting pH above 6.8, heating to denature protein, cooling and adjusting pH below 5.4.

DC D13

PA (NEZU-N) STICHT NED ZUIVELON

CYC 6

PI NL 8204923 A 19840716 (198432)* 13p <--

AU 8322583 A 19840628 (198433) <--

EP 115651 A 19840815 (198433) EN <--

R: DE FR GB NL

US 4519945 A 19850528 (198524) <--

EP 115651 B 19860820 (198634) EN <--

R: DE FR GB NL

DE 3365478 G 19860925 (198640) <--

ADT NL 8204923 A NL 1982-4923 19821221; EP 115651 A EP

1983-201707 19831130; US 4519945 A US 1983-562102 19831216

PRAI NL 1982-4923 19821221

REP FR 2130606; GB 2063273; GB 704209

IC A23C009-20; A23C021-06; A23J001-20

AB NL 8204923 A UPAB: 19930925

A ppte. of casein and whey protein is prep'd. from a milk prod. contg. these by (a) adjusting the pH of the material to over 6.8, (b) heating the resulting material for a combination of time and temp. above that at which the whey protein is denatured, (c) cooling the prod. to below 65 deg.C, (d) lowering the pH of the soln. to below 5.4 and (e) sepg. the resulting ppte.

Pref. (i) in stage (a) the pH is raised to 7.0-7.5 using a basic cpd. or an ion exchanger, and esp. NaOH; (ii) heating stage

(b) is carried out for 5-20 mins. at 80-100 deg.C, esp. 8-12 mins. at 90-98 deg.C, for 60 secs. at 130 deg.C or 5 secs. at 145 deg.C; (iii) in step (c) the mixt. is cooled to 4-45 deg.C; (iv) in step (d) the pH is lowered to 4.4-4.7; (v) pref. before sepg. the ppte. the prod. from step (d) is subjected to direct steam injection or indirect heating; (vi) the ppte. is washed with an aq. liquor at a pH of 4.2-5.4, esp. 4.4-4.7.

ADVANTAGE - The ppte. obtd. has excellent solubility in water at neutral pH, very low Ca content and low ash content. The low ash content and presence of **lactalbumin** makes the prod. esp. useful for the prodn. of baby foods.

0/0

FS CPI

FA AB

MC CPI: D03-B; D03-H01T

ABEQ EP 115651 B UPAB: 19930925

A process for the preparation of a precipitate of casein and whey protein from a milk product containing casein and whey protein, characterised in that (a) the pH of said milk product is adjusted to a value above 6.8, (b) the product obtained in step (a) is heated at a temperature and for a time at least sufficient to denature the whey protein, (c) the product obtained in step (b) is cooled to a temperature below 65 deg. C, (d) the pH of the cooled solution is reduced to a value below 5.4 and (e) the resulting precipitate is isolated.

ABEQ US 4519945 A UPAB: 19930925

Ppte. of casein and whey protein is prep'd. from a milk prod. contg. them, by (a) adjusting pH to more than 6.8; (b) heating prod. obtd. at temp. and time to at least denature whey protein; (c) cooling prod. to less than 65 deg.C; (d) reducing pH to less than 5.4; and (e) isolating ppte.

Pref. pH is adjusted in (a) with NaOH or non exchanger. Heating in (b) is carried out at 80-100 deg.C for 5-20 mins. or at 130 deg.C for 60 secs., or 145 deg.C for 5 secs. Cooling temp. is 4-45 deg.C. Ppte. obtd. in (d) is subjected to direct steam injection or indirect heating before isolating prod..

ADVANTAGE - Prod. has low Ca-content (0.1 wt.%) and high protein solubility (i.e. 95%).

L114 ANSWER 17 OF 17 WPIX (C) 2003 THOMSON DERWENT

AN 1970-81117R [44] WPIX

TI Fractionated milk components for animal - feedstuffs prepn.

DC D13

PA (MOL-N) MOLKEREI MEGGLE JA

CYC 2

PI DE 1492803 B (197044)*
NL 138857 B (197322)

PRAI DE 1965-M604270 19650222

IC A23C000-00; A23K000-00

AB DE 1492803 B UPAB: 19930831

Milk is soured by **ion-exchange** treatment and fractionated by acid pptn. of casein. Heat treatment to concentrate the whey, crystalliser of milk sugar (lactose) and removal of **lactalbumin** is effected. Addition of albumin to the whey concentrate forms the basis of an aminal feed with carbonates and hydroxides added.

FS CPI

FA AB

MC CPI: D03-B; D03-G

=> d his

FILE 'HCAPLUS' ENTERED AT 11:08:43 ON 27 MAR 2003

	E LACTALBUMIN/CT
L1	3145 S E5-E7
	E E4+ALL
L2	4150 S E3
L3	8 S E4-E7/B1
	E LACTALBUMIN
L4	6055 S E3
	E LACTALBUM
	E LACTALBU
	E LACTALB
L5	15 S E2,E4-E12
L6	8 S E14-E20
L7	1 S E33
L8	6071 S L1-L7
L9	160 S L8 AND ?OLIGO?

FILE 'REGISTRY' ENTERED AT 11:12:38 ON 27 MAR 2003

	E LACTALBUMIN/CN
L10	1 S E7
L11	111 S LACTALBUMIN(S) ALPHA
L12	115 S LACTALBUMIN

FILE 'HCAPLUS' ENTERED AT 11:13:55 ON 27 MAR 2003

L13	65 S L10-L12
L14	6075 S L8,L13
L15	4242 S L14 AND ALPHA
L16	143 S L15 AND ?OLIGO?
L17	239 S L14 AND MOLT?
L18	2592 S L14 AND ?GLOBUL?
L19	39 S L16 AND L17,L18
L20	50 S L15 AND POLYMERIZ?
L21	32 S L20 AND L17,L18
L22	66 S L19,L21
	E SVANBORG C/AU
L23	126 S E3-E8
	E SVANBOERG C/AU
	E HAKANSSON P/AU
L24	66 S E3,E6,E7
	E SVENSSON M/AU
L25	62 S E3,E13,E15
	E HAKANSSON A/AU
L26	48 S E3-E7
L27	13 S L23-L26 AND L14
L28	3 S L27 AND ION(S)CHROMATOG?(S)EXCHANG?
L29	3 S L28 AND L15-L22
	E ION EXCHANGE/CT
	E E3+ALL
L30	21903 S E3+NT
	E E11+ALL
L31	6940 S E4+NT
	E E45+ALL
L32	42249 S E5,E4+NT
L33	76 S L14 AND L30-L32
L34	76 S L33 AND L14
L35	143 S L14 AND (ION OR ANION)(S)EXCHANG?(S)CHROMATOG?
L36	124 S L15 AND L35
L37	161 S L33-L36
	E CASEIN/CT
	E E3+ALL
L38	25 S L37 AND E1,E2
	E E2+ALL
L39	39 S L37 AND CASEIN

L40 39 S L38,L39
 L41 2 S L40 AND CHELAT?
 L42 1 S L40 AND EDTA

FILE 'REGISTRY' ENTERED AT 11:31:22 ON 27 MAR 2003

L43 1 S 60-00-4
 L44 1 S 7647-01-0
 L45 436 S 60-00-4/CRN
 L46 1 S 1185-53-1
 L47 1 S 77-86-1
 L48 942 S 77-86-1/CRN
 L49 1 S 112-80-1
 L50 2556 S 112-80-1/CRN
 L51 757 S L50 AND 2/NC AND C18H34O2 NOT IDS/CI
 L52 687 S L51 NOT UNSPECIFIED
 L53 1 S 7647-14-5
 L54 1 S 80701-61-7
 E DEAE/CN
 L55 2 S E33,E34

FILE 'HCAPLUS' ENTERED AT 11:33:40 ON 27 MAR 2003

L56 1 S L43,L45 AND L37
 L57 3 S L44 AND L37
 L58 1 S L47,L48 AND L37
 L59 1 S L49,L52 AND L37
 L60 8 S L53 AND L37
 L61 1 S L54,L55 AND L37
 L62 8 S L56-L61
 L63 180 S L1(L) PREP?/RL OR L2(L) PREP?/RL
 L64 5 S L63 AND L62
 L65 5 S L64 AND ALPHA
 L66 4 S L65 NOT ANX/TI
 L67 6 S L29,L66
 L68 4 S L62 AND L67
 L69 6 S L67,L68
 L70 136 S L37 AND (PY<=1998 OR PRY<=1998 OR AY<=1998)
 L71 25 S L70 AND L63
 L72 21 S L71 NOT L69
 L73 20 S L72 AND ALPHA (S) LACTALBUM?
 SEL DN AN 1 7 9 10 16
 L74 15 S L73 NOT E1-E15
 L75 21 S L69,L74
 L76 110 S L70 NOT L71-L75
 L77 0 S L76 AND CHELAT?
 L78 1 S L76 AND (L43,L45 OR EDTA OR ETHYLENEDIAMINETRETRA? OR ETHYLEN
 L79 21 S L75 AND L1-L9,L13-L42,L56-L78
 L80 28 S L63 AND (?OLIGO? OR ?POLYM? OR ?MULTIMER?)
 L81 11 S L80 AND L37
 L82 8 S L70 AND L81
 L83 2 S L82 NOT L79
 L84 23 S L75,L82
 L85 2 S L84 NOT L75
 L86 21 S L84 NOT L85

FILE 'HCAPLUS' ENTERED AT 12:05:57 ON 27 MAR 2003

FILE 'WPIX' ENTERED AT 12:06:43 ON 27 MAR 2003

E LACTALBU
 L87 336 S E2,E4-E8/BIX
 E SVANBORG C/AU
 L88 6 S E3,E4,E5
 E SVANBEORG C/AU
 L89 1 S E25

E HAKANSSON /AU
L90 12 S E4
L91 17 S E40,E41
E SVENSSON M/AU
L92 38 S E3,E7
L93 1 S E66
E MALIN/AU
L94 3 S E62
L95 106 S C07K014-76/IC, ICM, ICS
L96 145 S A61K038-38/IC, ICM, ICS
L97 4 S L88-L94 AND L87,L95,L96
L98 545 S L87,L95,L96
L99 1 S L98 AND N152/M0,M1,M2,M3,M4,M5,M6
L100 40 S L98 AND (ION OR ANION)(S)EXCHANG?/BIX
L101 74 S L98 AND (OLIGO? OR MULTIMER? OR MULTI-MER? OR POLYMER?)/BIX
L102 44 S L98 AND CHROMATOOG?/BIX
L103 12 S L100,L102 AND L101
L104 445 S L98 AND (PY<=1998 OR PRY<=1998 OR AY<=1998)
L105 46 S L100,L102 AND L104
L106 10 S L101 AND L105
SEL DN AN 1 3 7
L107 3 S E1-E6
L108 6 S L97,L99,L107
L109 276 S L87 AND L104
L110 22 S L109 AND L105
L111 19 S L110 NOT L108
SEL DN AN 2 3 8 12 13 15 17 18
L112 11 S L111 NOT E7-E22
L113 14 S L108,L112 AND ALPHA
L114 17 S L108,L112,L113

FILE 'WPIX' ENTERED AT 12:35:49 ON 27 MAR 2003